

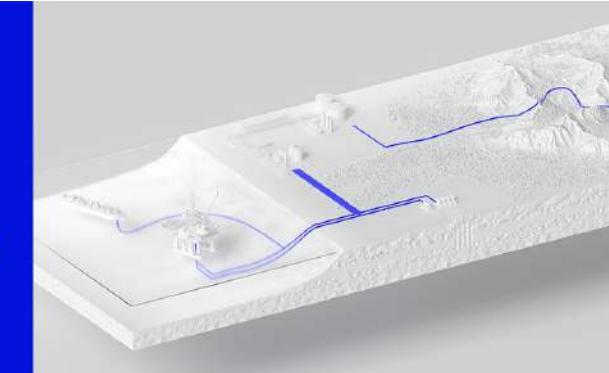


Holistic Models: Offshore Artificial Lift Training Simulator



Olga and Pipesim
User Group Meetings

October 2025 – March 2026



inprocess

Since 2006 helping the processing industries in solving design and operational issues by applying process simulation

our **core business** is Process Simulation

enthusiastic about **sharing our knowledge** with our clients

all technologies (process simulator and control system)



2006

est. in Barcelona by domain experts



Projects in 55 countries

worldwide presence



110+

process simulation engineers



400+

executed projects



>90

OTS Projects



330+

training courses

Inprocess Solutions & Services



Engineering Studies



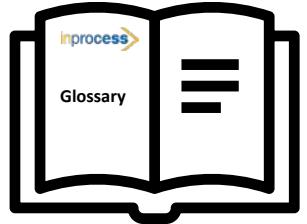
Operator Training



Digital Twins



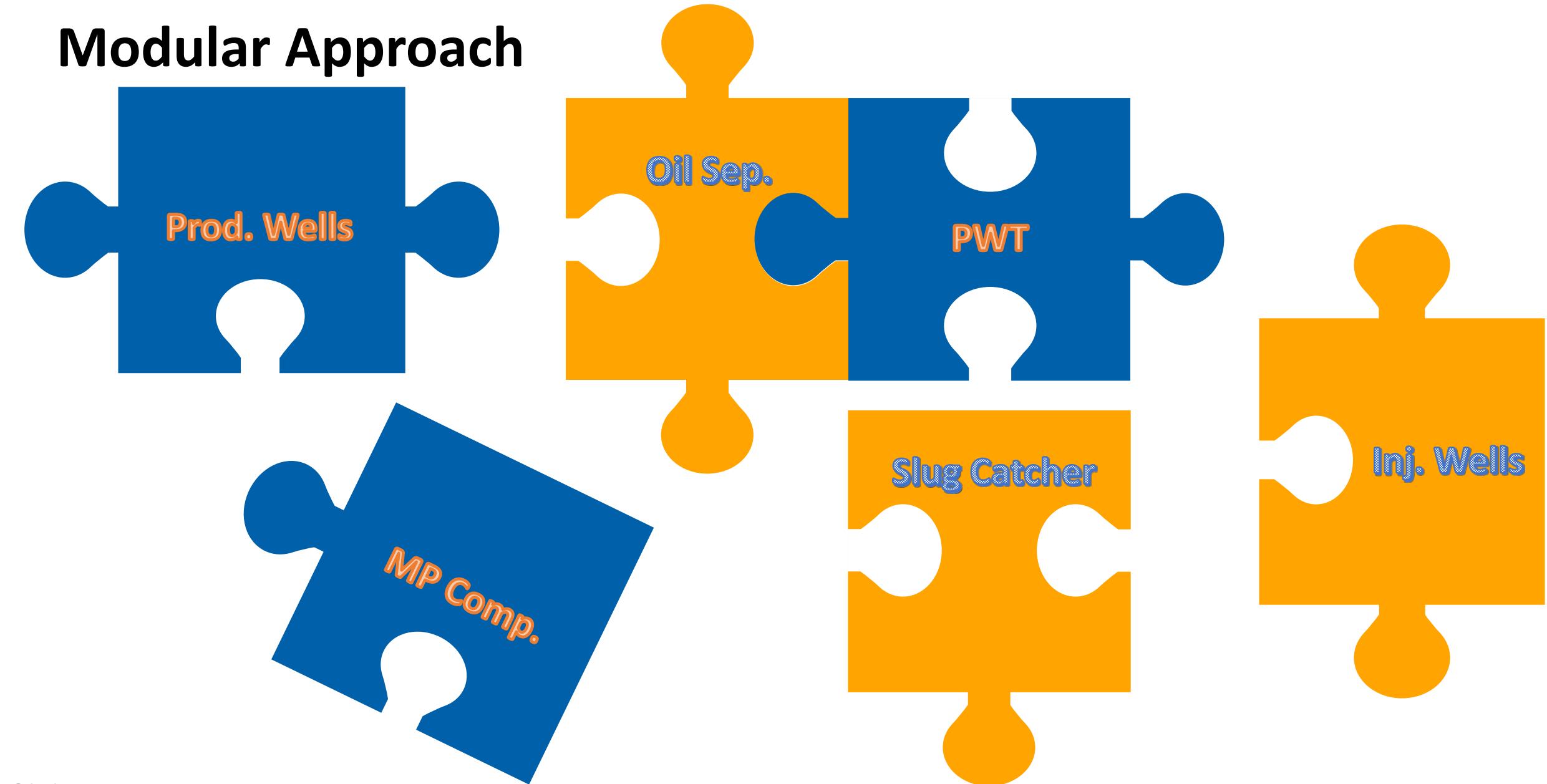
Engineering Training

**Holistic (Adjective):**

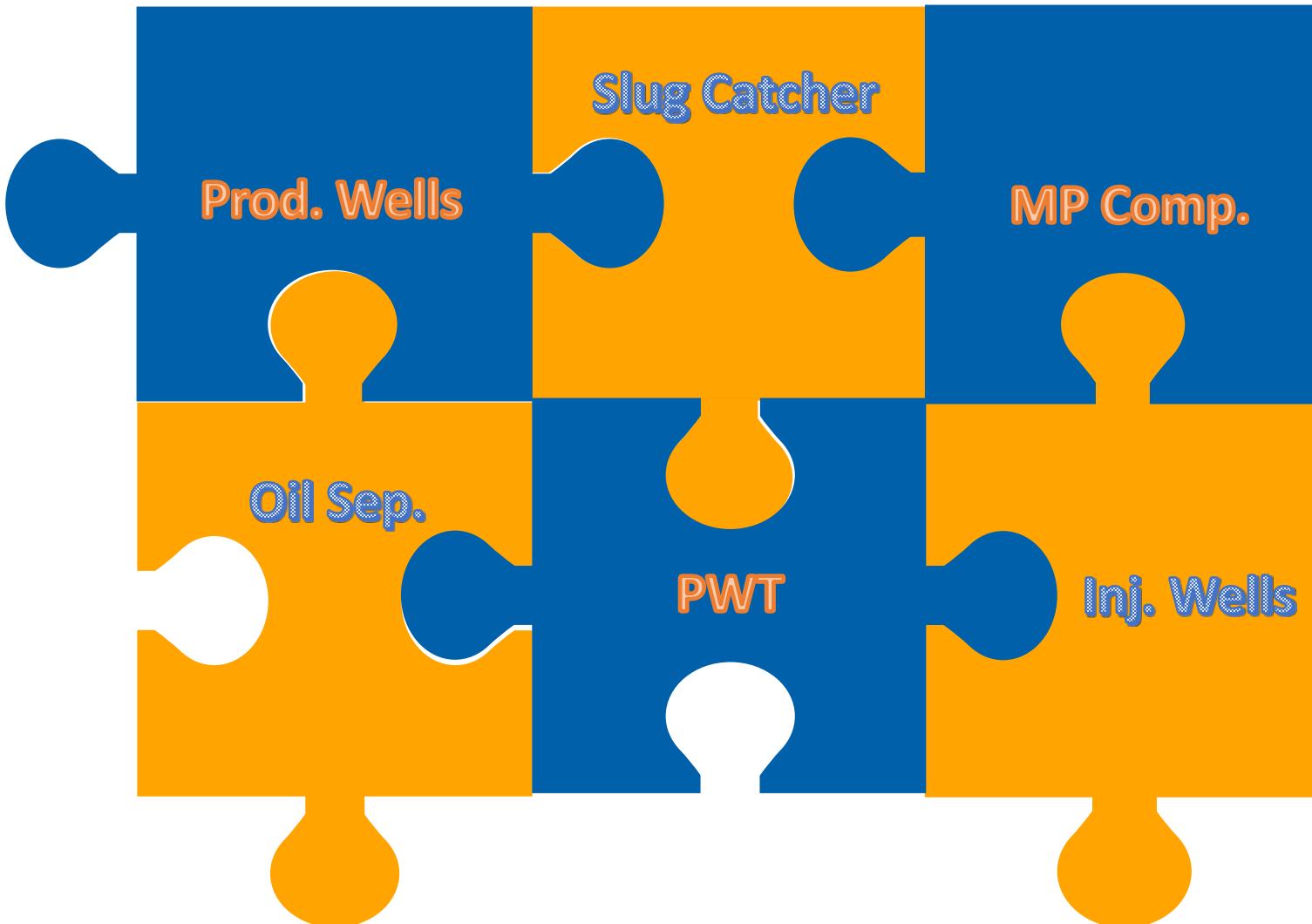
Characterized by the belief that the parts of something are interconnected and can be explained only by reference to the whole.

- A modular dynamic simulation approach considers each unit as an individual entity.
- A holistic dynamic simulation approach takes into account the interconnectivity between all units.
- Holistic simulations can also link **process simulator** (e.g. Symmetry) software with **flow assurance software** (e.g. Schlumberger OLGA) to take advantage of the best from both worlds.

Modular Approach



Holistic Approach



Modular Approach



- Each unit is analysed independently.
- Standalone simulation models.
- OLGA outputs used as inputs.
- Less computational cost, greater RTF.

Holistic Approach

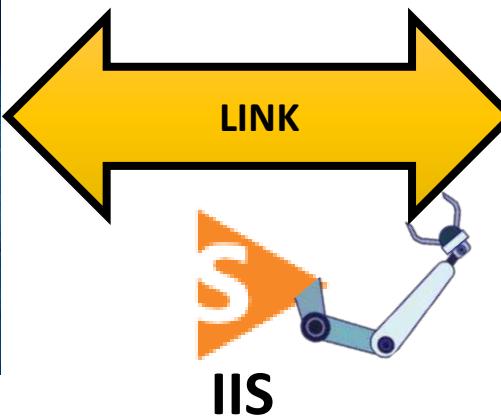
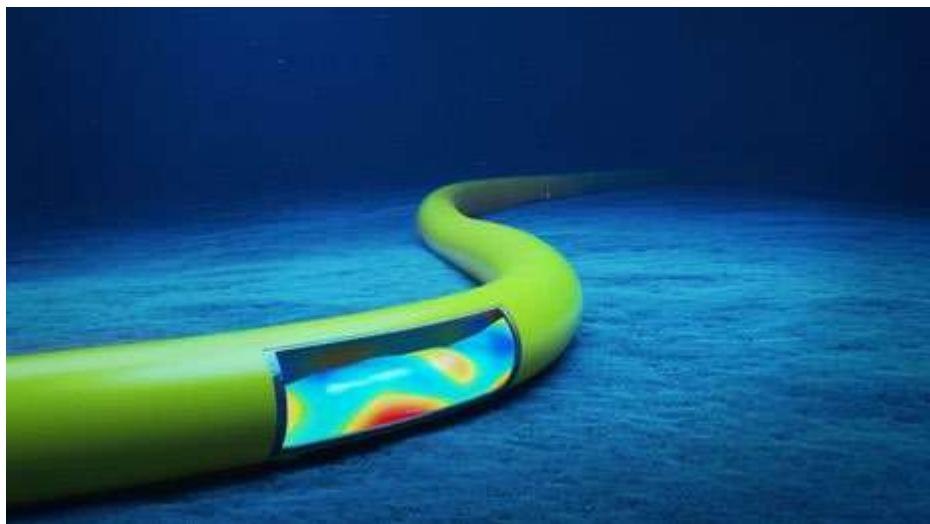


- Interaction between units is analysed.
- One integrated simulation model.
- OLGA and Process Model Linked
- More computational cost, lower RTF.

$$RTF: \text{Real time factor} \rightarrow RTF = \frac{\text{Simulated time}}{\text{Real Time}}$$

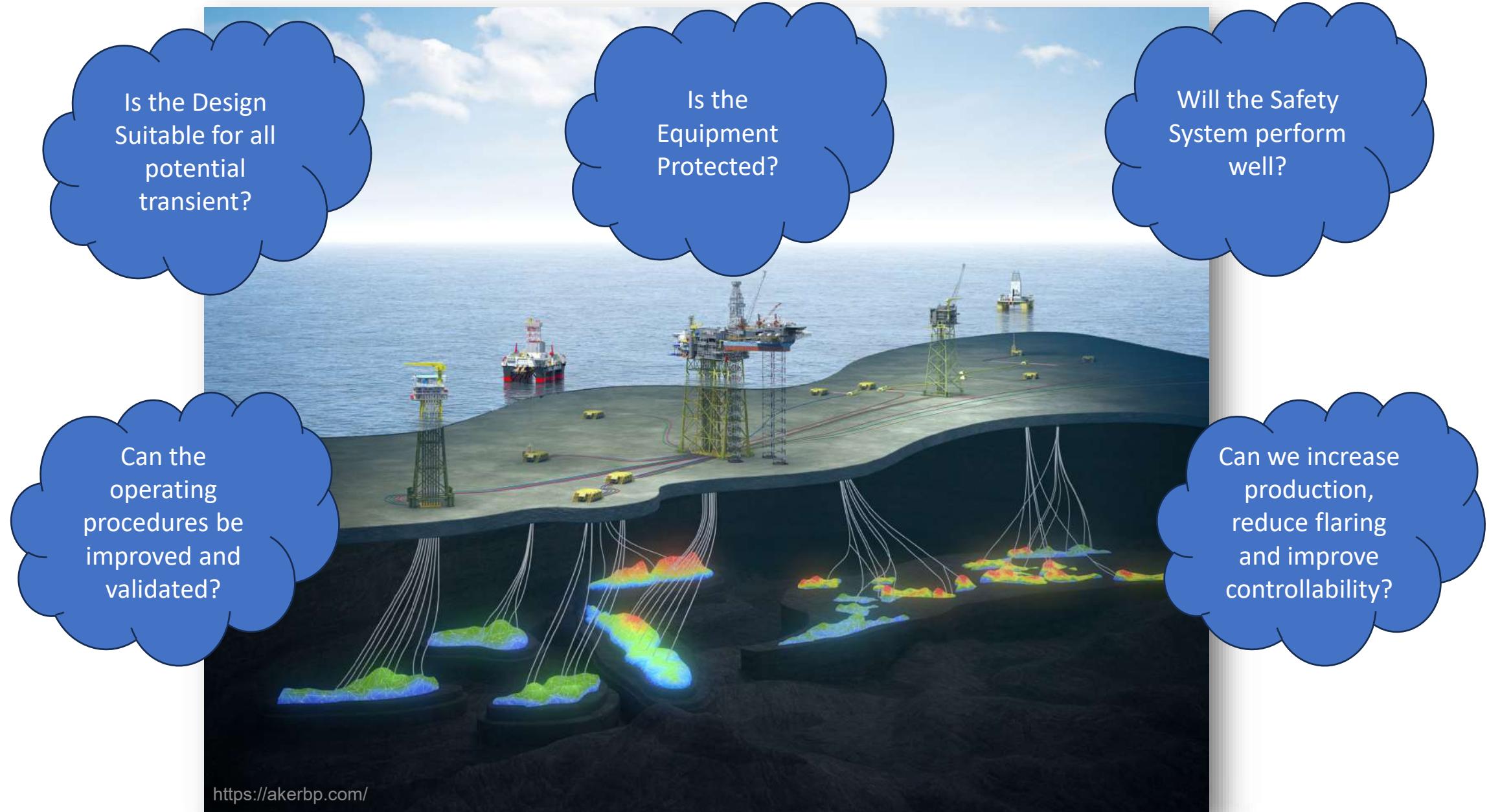
- ▶ Facilities models and OLGA model share information using OPC protocol.
- ▶ Inprocess Infrastructure Suite (IIS) application manages the communication and synchronization between models.
- ▶ IIS allows starting/stopping simulation, saving/loading snapshots, plot trends, etc.

OLGA Model



Process Simulator Model





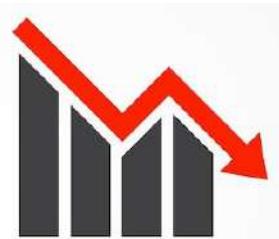


Case Study #1 - Offshore Artificial Lift Training Simulator



Background & Motivation

- Offshore operator facing production decline in **aging subsea wells**.



- Decision made to install subsea **Electrical Submersible Pumps (ESPs)** — a first for their offshore team, though ESPs are common in their onshore assets.



- Operators had **no prior experience** with ESP operations, start-up, or shutdown procedures.



- ESPs project to extend field life expectancy beyond 2050, **recovering billions** in potential production value.





Inprocess Approach

➤ Holistic Simulation:

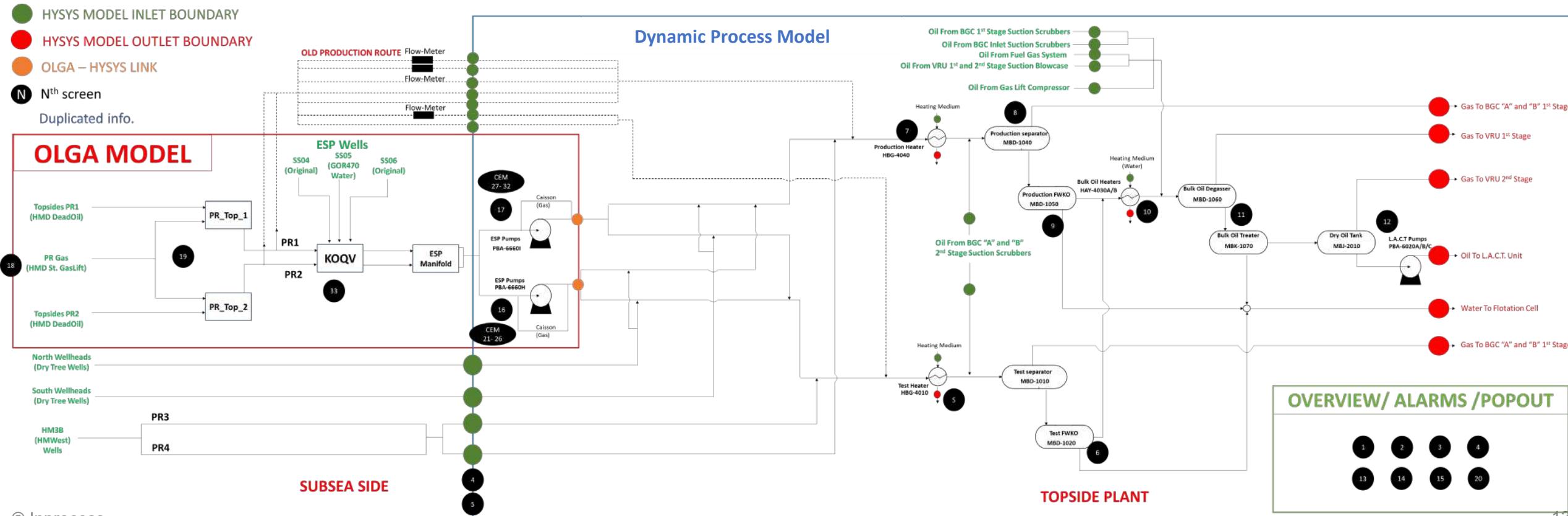
- Topside process modelled in dynamic simulation process simulator.
- Subsea network modelled in OLGA.
- Integration achieved through Inprocess' proprietary linking interface for seamless dynamic data exchange.



Inprocess Approach

Holistic Simulation:

- Topside process modelled in dynamic simulation process simulator.
- Subsea network modelled in OLGA.
- Integration achieved through Inprocess' proprietary linking interface for seamless dynamic data exchange.





Inprocess Approach

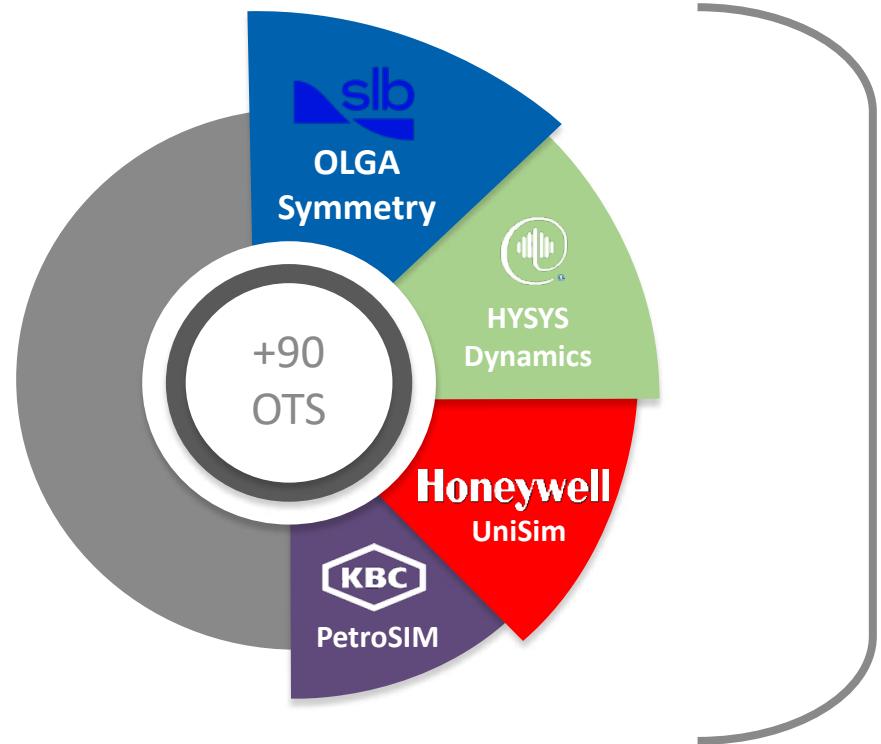
➤ Holistic Simulation:

- Topside process modelled in dynamic simulation process simulator.
- Subsea network modelled in OLGA.
- Integration achieved through Inprocess' proprietary linking interface for seamless dynamic data exchange.

➤ The OTS was configured to simulate all operational modes:

- Normal and abnormal start-up sequences.
- Subsea equipment malfunctions.
- ESP trips and shutdown recovery scenarios.

Dynamic Process Simulation Technology



Inprocess Infrastructure Suite (IIS)

Through,

DCOM (i.e. commands)

OPC DA

OPC UA

CORBA

Proprietary Protocols (i.e. ExaTIF)

Windows Fundation

(i.e. SIEMENS SIMIT commands)

ICSS Technology

- EMERSON Delta V
- SIEMENS PCS7 and APACS/Quadlog
- Yokogawa Centum VP
- ABB 800xA
- Honeywell Experion PKS and TPS
- Kongsberg Maritime K-Chief 700
- Schneider-INVENSYS Foxboro I/A
- Rockwell
- CCC
- GE Mark
- Generic ICSS emulators

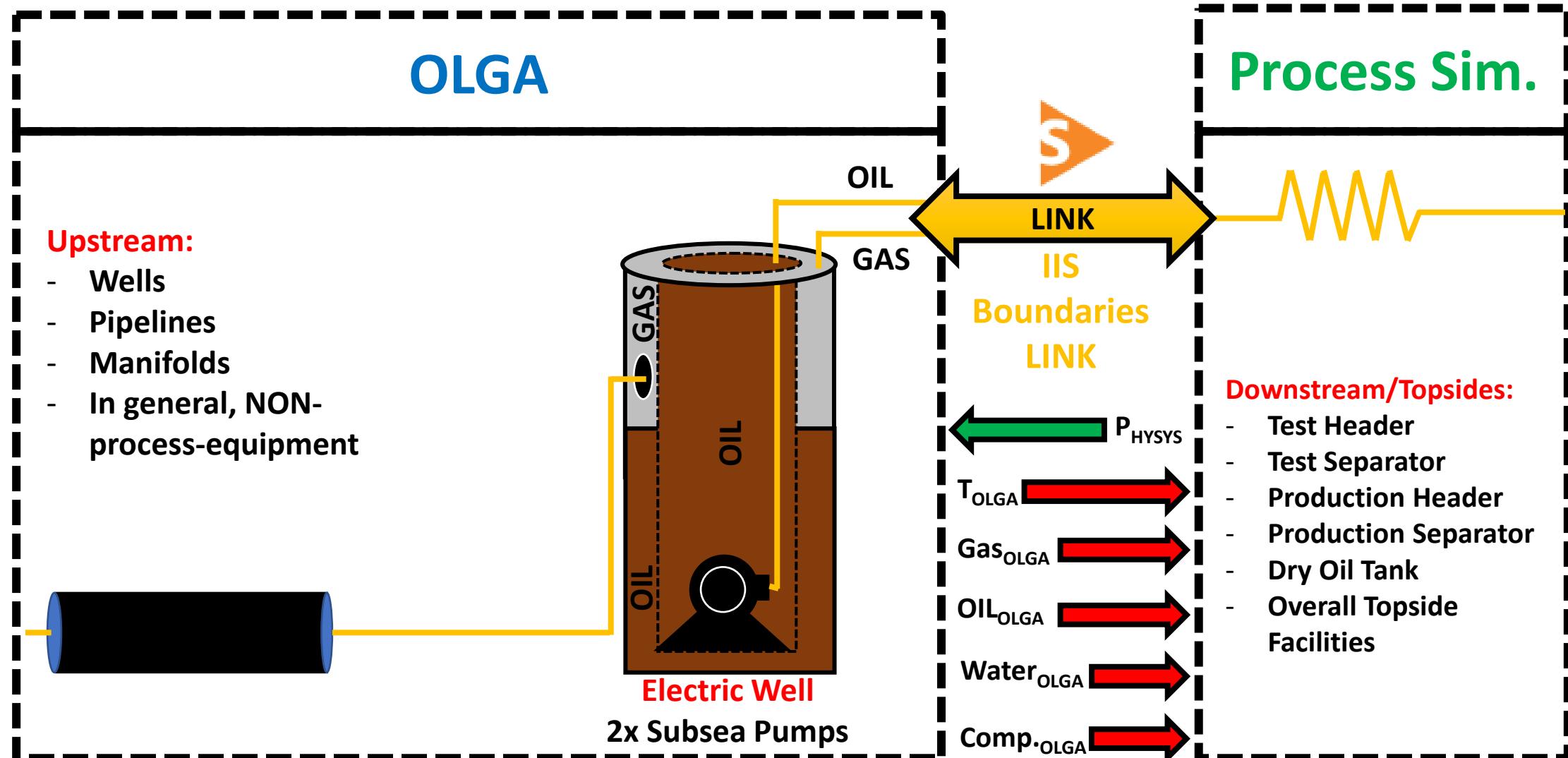
PLANT HISTORIANS

- OSI PI, Honeywell's PHD, Azure's IoT Hub, OPC server, etc.

OTHERS

- Excel
- Other communication protocols can be developed on demand.

- Simulation speed of both Software's is controlled and synchronized by IIS link.
- Data transfer between software's is performed via OPC protocol.





Project Challenges & Solutions

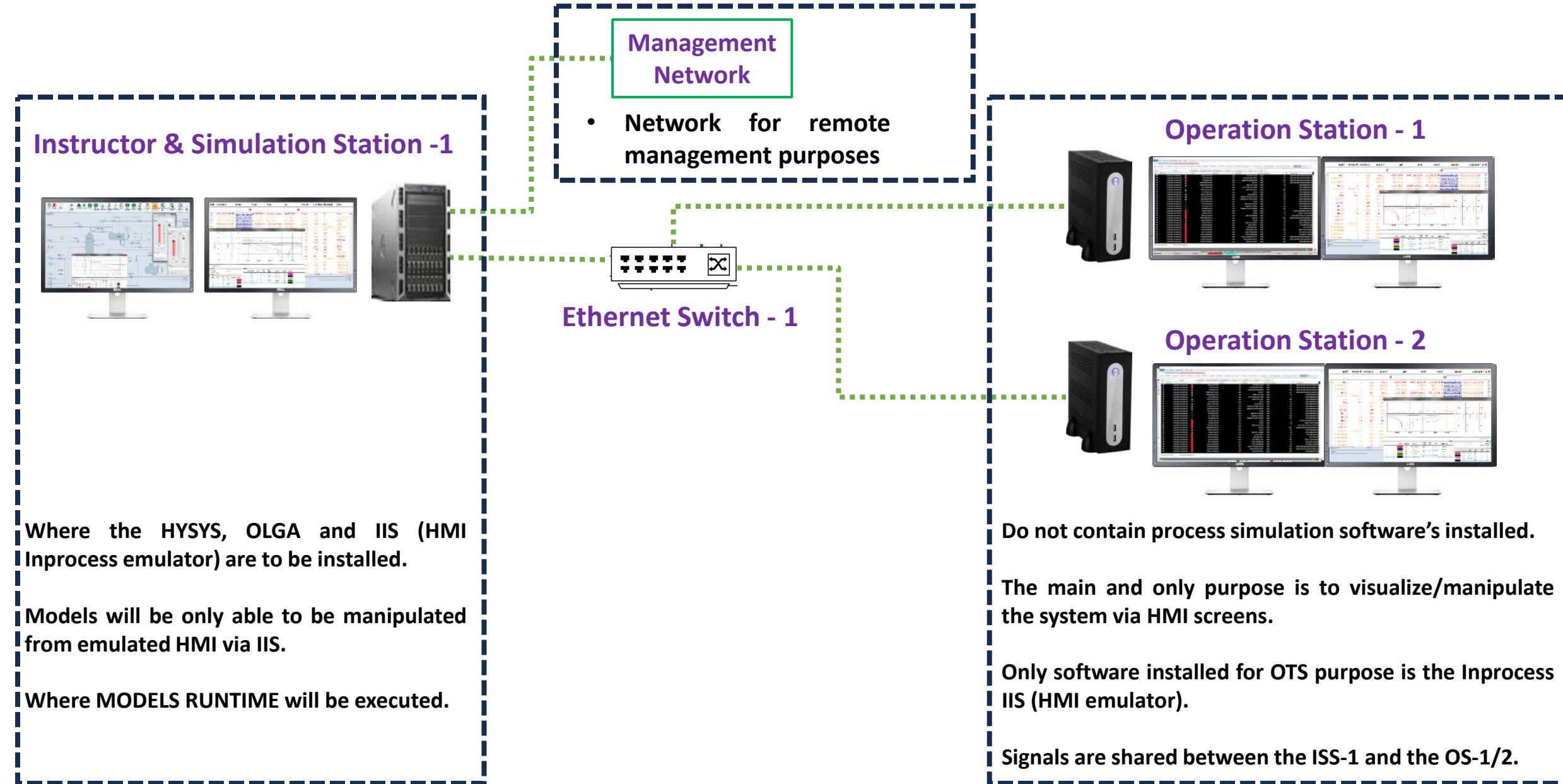
Operators provided hands-on feedback that led to:

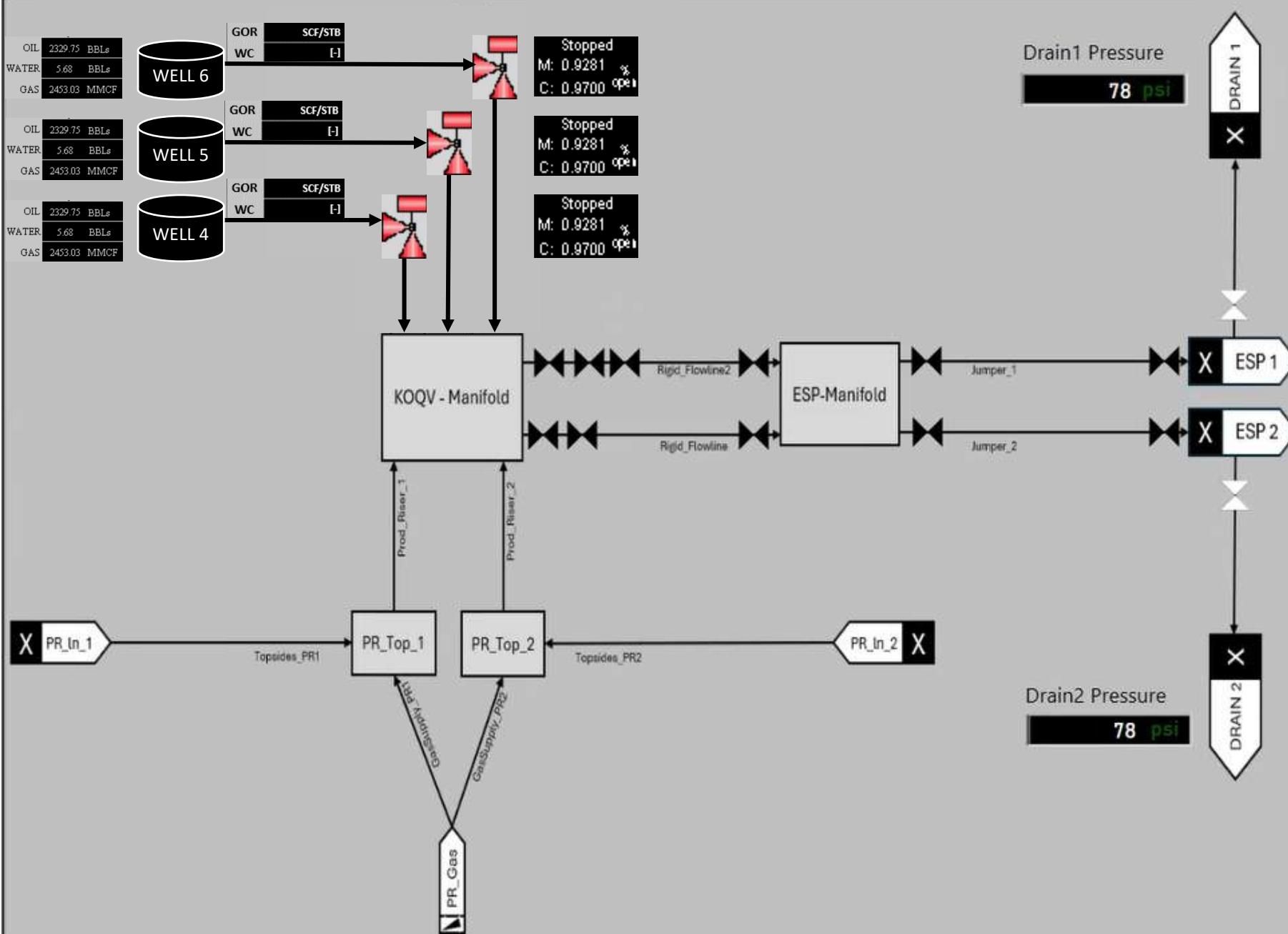
- Major revisions in start-up and shutdown procedures. Engineering assumptions proved unrealistic under real conditions and operator experience.

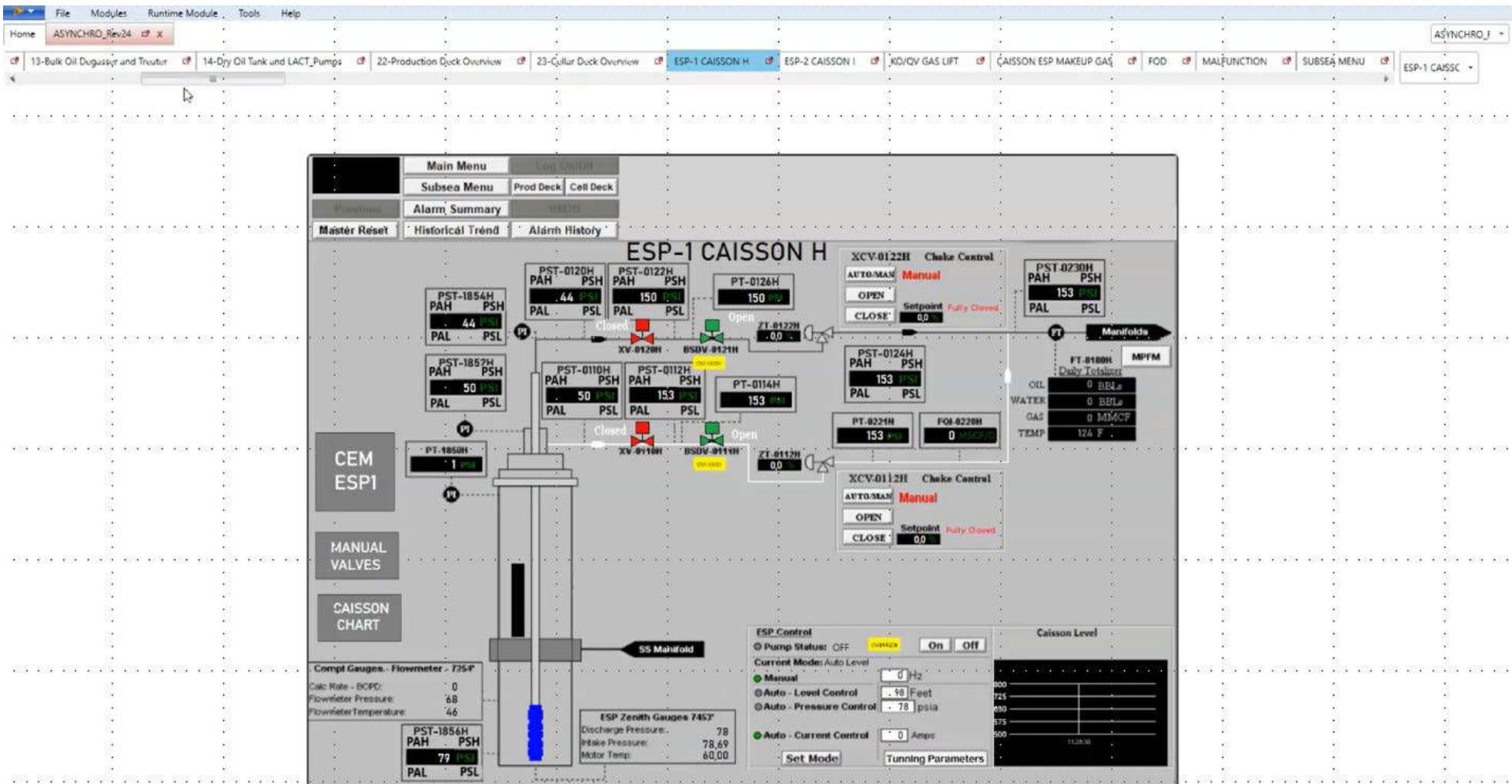
OTS caught an error for ESP control. Narrative stated it should be based on discharge pressure.

Walking through the scenario with the ESP consultants highlighted that this should be on suction pressure.

INPROCESS SEQUENCE				ORIGINAL SEQUENCE
#	ELEMENT	ACTIONS	REASON	
1	XV0110H XV110L	OPEN —	Maintain the pressure in the gas line, avoid depressurisation of the line due to condensation	1 LOW HZ FOR PREHEAT
	P0650M P0650P	AUTO KC=1 T1=1 SP=200	Help driving force	2 WAIT TO 100F ON THE CAISSON
	PR1 PR2 MF 70000 lb/h	—	Feed the system, packing with dead oil until level is achieved	3 STOP PREHEAT MODE
	CAISSON	ON HZ=20	Preheat wait to 100F on the caisson	4 OPEN DEAD OIL UNTIL LEVEL IS ACHIEVED
	WAIT UNTIL LEVEL IN CAISSON IS STABLE			5 CAISSON HZ=40
2	CAISSON ESP	HZ=64	Main purpose of step 1 is to fill caisson and to preheat the pump Fill the downstream caisson system. Against the top sides closed valves	6 OPEN ALL TOP SIDE WELL HEAD VALVES (XV, BSDV AND CHOKE)
	WAIT TO HZ=64			7 IF THERE IS NO FLOW IN 2 MIN, STOP CAISSON
3	CHOKE CONTROL 100	ESP1= ESP2= 80	ESP2 choke control has to remain more closed than ESP1. This is due to the difference in caissons heights and to balance the hydraulics. This will let both pumps to discharge at same time to bypasses.	8 RUN UNTIL 160F IS ACHIEVED
	XV0110 / 0120	OPEN —	Open export line to topsides	9 OPEN WELL AND MIX WITH DEAD OIL
	WAIT UNTIL PRODUCTION IS ACHIEVED			10 SLOWLY CLOSE DEAD OIL AND OPEN WELL PRODUCTION
4	PR1 PR2 MF 50% OPEN	0 lb/h	If 6 min (check FT-3110) of dead oil production are considered, system will push the dead oil to topsides. After that dead oil to close and wells to open	11 GRADUALLY INCREASE ESP SPEED
	WELLS 4,5,6	—	Dead oil is sent to close gradually or suddenly Wells are opened gradually or suddenly	12 SWITCH FROM MAN MODE TO LC CONTROLLER
5	WELLS 4,5,6	100% OPEN	Wait to an increase of the production Once well production arrives to the caisson, an increase of the production is going to be noticed	
	FULL PRODUCTION AND END OF THE COLD START UP - ACHIEVEMENT OF SS CONDITIONS ALL CAN BE TURNED INTO AUTO MODE			







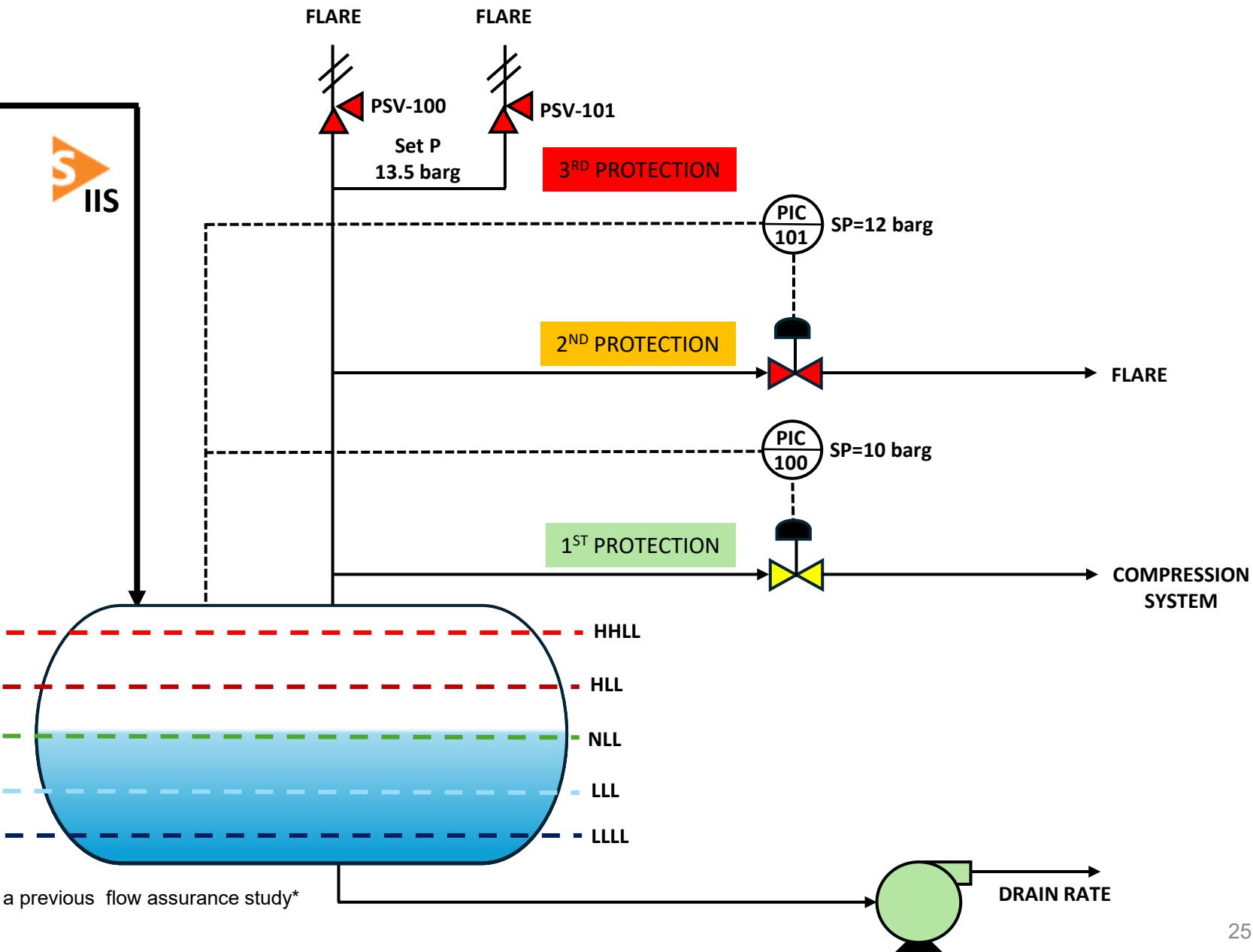
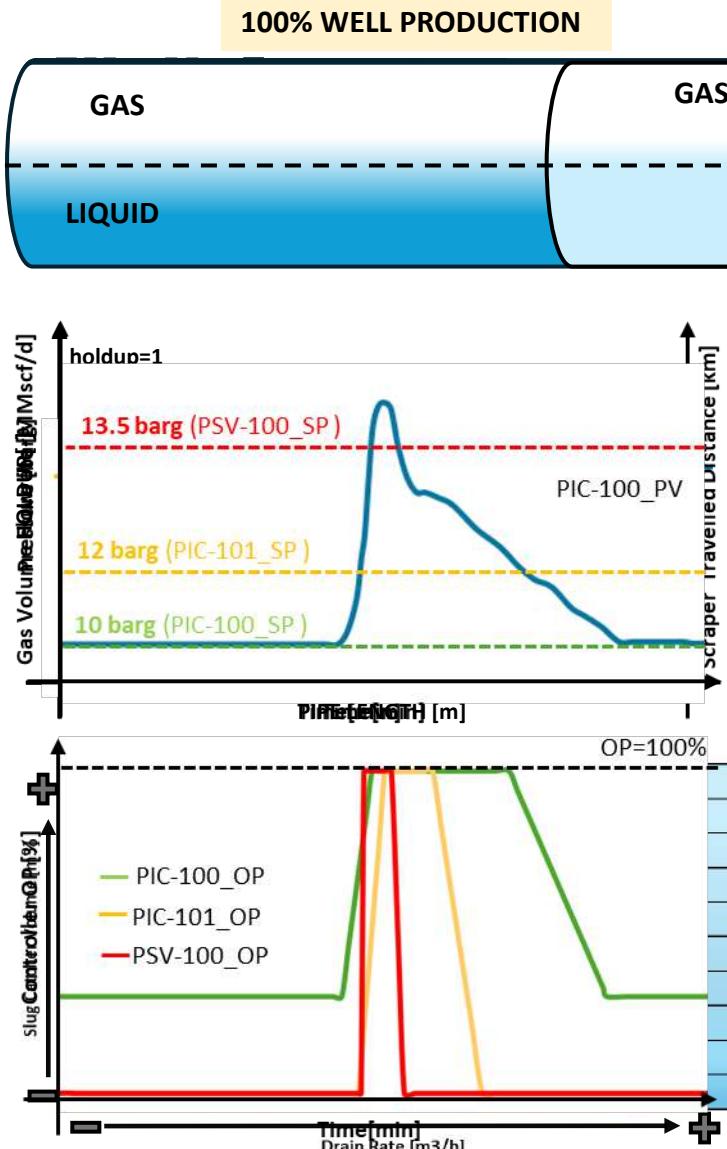
In this video, we will demonstrate how to start up a caisson using an OTS (Operator Training Simulator).



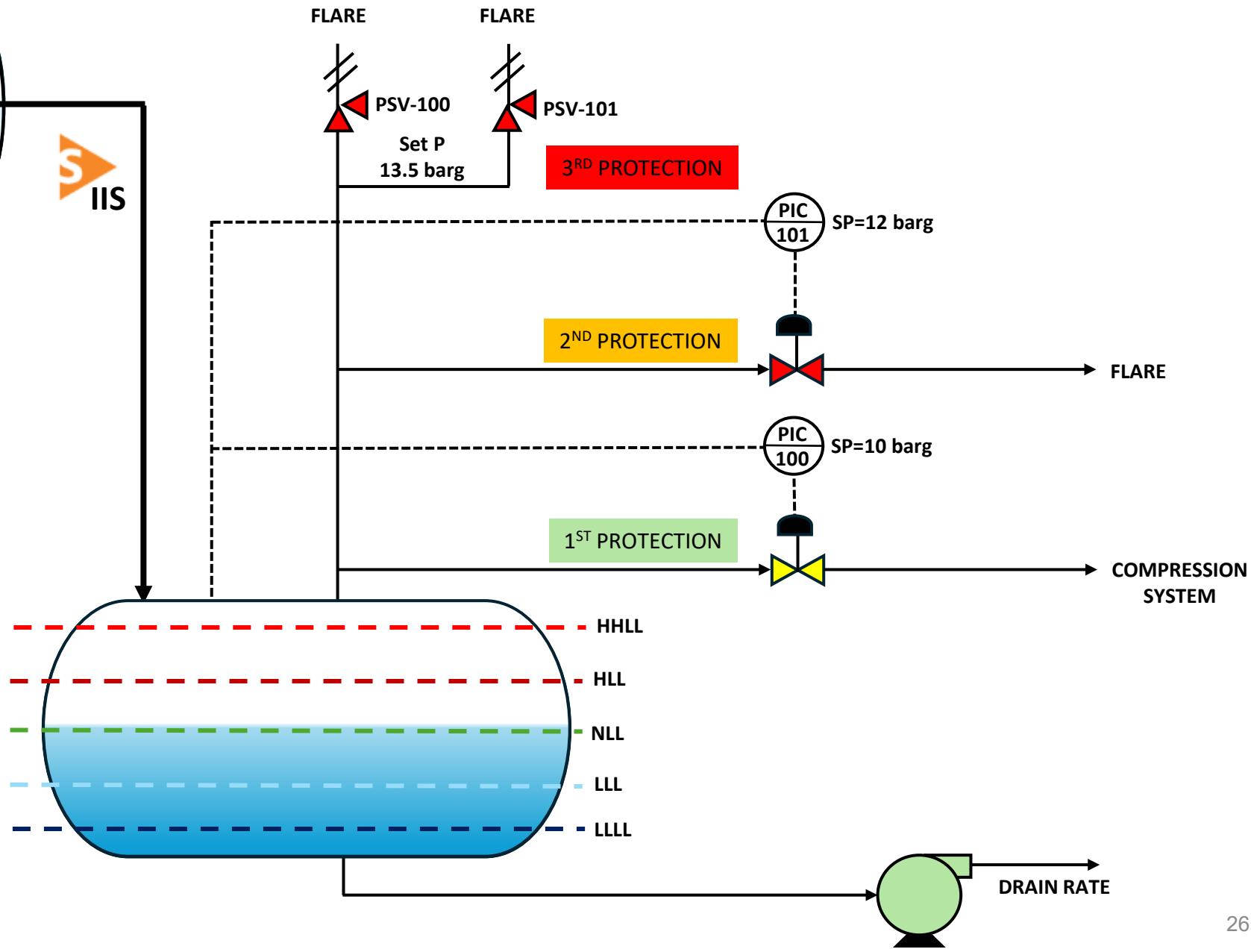
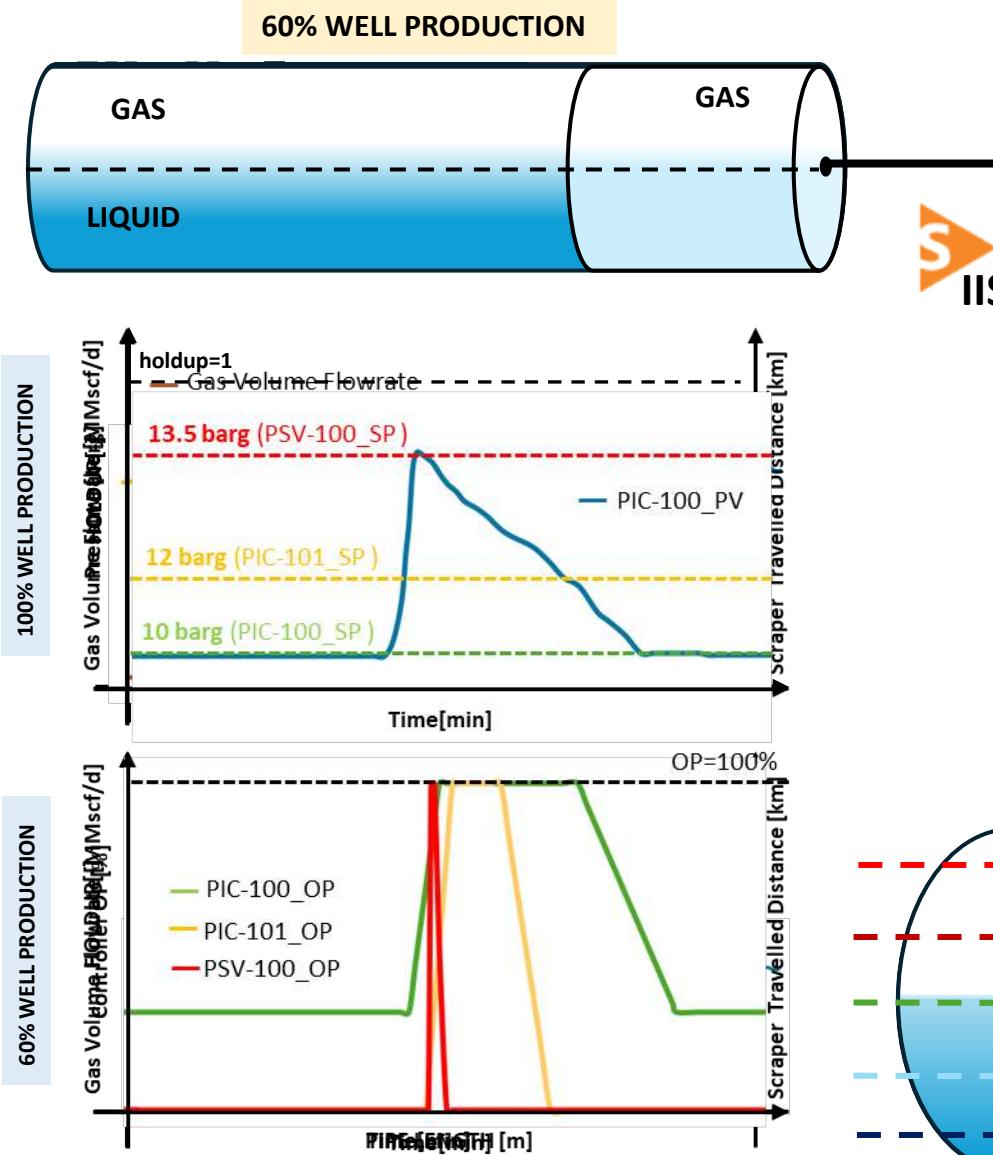
Project Benefits

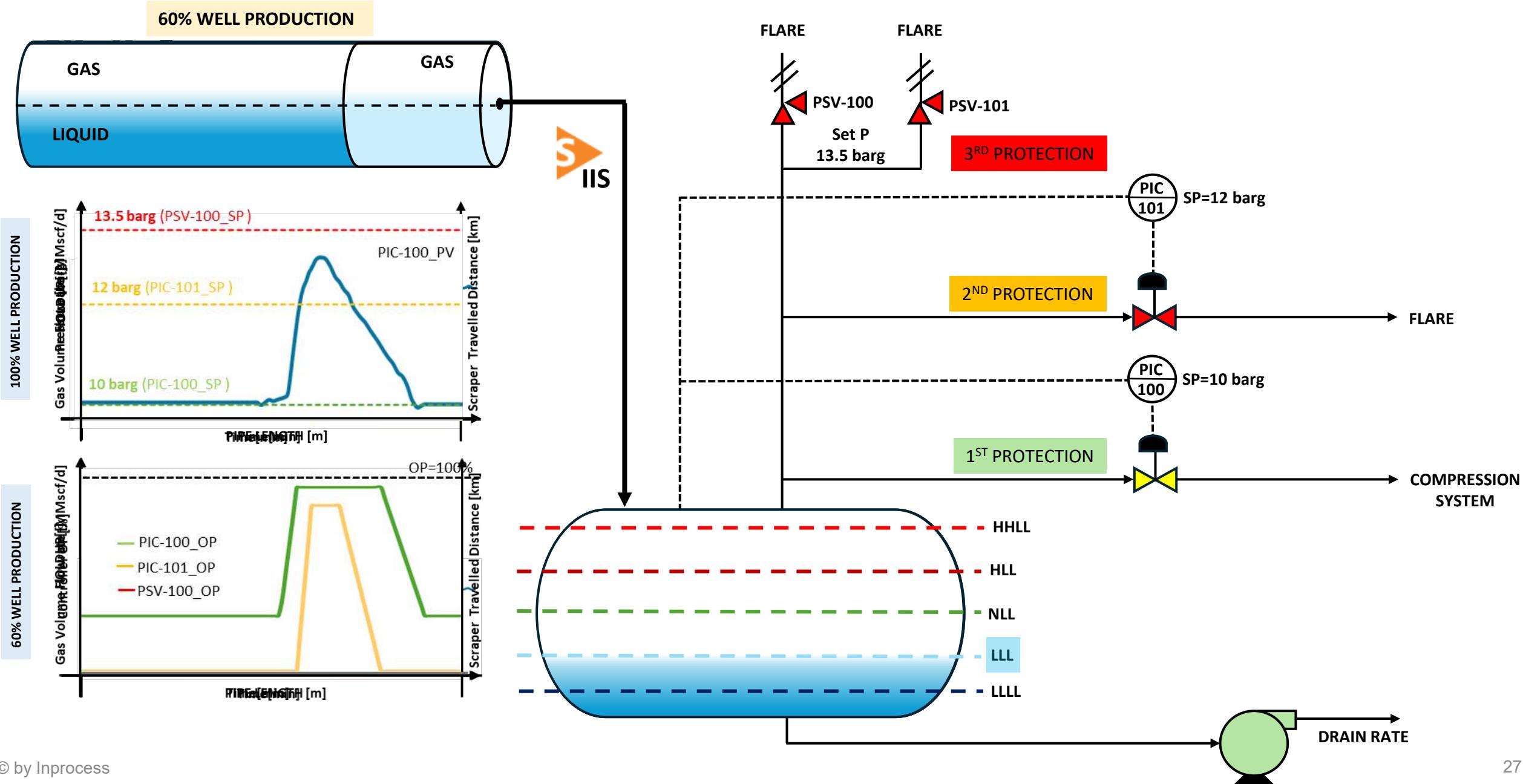
- Conducted 10+ **training sessions** across operating shifts to ensure broad engagement.
- OTS became a **procedure validation** tool, not just a training platform.
- OTS was able to adjust **tuning parameters** for ESPs in advance of startup.
- OTS caught an error for ESP control. **Narrative** stated it should be based on discharge pressure. Walking through the scenario with the ESP consultants highlighted that this should be on suction pressure.
- **Developed HMI** screens in parallel with control system supplier (ahead of schedule) and were tested within the simulator environment to capture operator feedback before final deployment.
- Facilitated **cross-discipline collaboration** between engineering, operations, and control system teams.
- Validated that **dead oil** circulation is only required during initial startup, not for every restart which significantly reducing offshore operational effort.
- **The actual start-up went flawlessly, and production has increased by 5,000 BPD with only one pump online.**

Case Study #2 - Slug Catcher analysis during scraping operation



Only the drain rate was considered to size the Slug Catcher according to a previous flow assurance study*





General conclusions

- ✓ Avoided the opening of PSVs.
- ✓ Avoided trips in the Slug catcher and downstream facilities during scraping operations.

Holistic Approach benefits for scrapping operations

- ✓ Analyzing controller response during scraping operations.
- ✓ Validate Slug Catcher dimensions during scraping operations.
 - Only the drain rate was considered to size the Slug Catcher according to the flow assurance study. However, the holistic dynamic simulation study proves that the dimensions of the Slug Catcher were not enough to prevent the opening of the PSVs due to the accumulated gas in the pipeline during the scrapping operation.
- ✓ Parametric study of the well production
 - ✓ The reduction of the wells production was crucial to decrease the amount of gas accumulated behind the scrapper. However, it is important to keep enough flowrate to guarantee that the scraper is not trapped in the pipeline.

Thank you!

Q&A

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