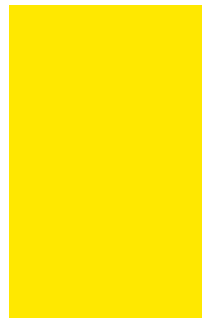


YINSON
PRODUCTION



Lifecycle Aspen HYSYS Modelling for FPSO, from Engineering Studies to OTS



Lifecycle Aspen HYSYS Modelling for FPSO, from Engineering Studies to OTS



Kari Berte Bye (Yinson)

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A more comprehensive discussion of the risk factors that may impact Yinson’s business can be found in the Group’s latest Annual Report, a copy of which can be found on the Group’s corporate website, www.yinson.com.my

Agenda

Yinson and Eni's OCTP Project

- Motivation for Lifecycle dynamic modelling
 - Phase 1: Process Design & Control Validation
 - Phase 2: Procedures Verification & Early Senior CRO's Training
 - Phase 3: ICSS Database Checkout
 - Phase 4: Operator Training System
 - Phase 5: FPSO Start-up Support
- Operator competency training program
- Yinson's approach to Lifecycle
- Conclusions





YINSON
PRODUCTION

Yinson Production – Our Fleet



FPSO Name FPSO Allan
Charterer CNR
Field Olowi, Gabon
Storage Capacity 1.04 million barrels
Production Capacity:
Oil 35,000 BOPD
Liquid 50,000 BLPD
Gas Compression 75 MMSCFD
Contract Duration 2009 – 2019 (2029)
Ownership 100% YINSON



FSO Name PTSC Bien Dong 01
Charterer PetroVietnam
Field Block 05-2/05-3, Vietnam
Storage Capacity 350,000 barrels
Contract Duration 2013 – 2023 (2033)
Ownership 51% PTSC, 49% YINSON



FPSO Name FPSO Adoon
Charterer Addax Petroleum
Field Block OML 123, Nigeria
Storage Capacity 1.7 million barrels
Production Capacity:
Oil 60,000 BOPD
Liquid 140,000 BLPD
Water Injection 50,000 BWPD
Gas Compression 7 MMSCFD
Contract Duration 2006 – 2018 (2022)
Ownership 100% YINSON



FPSO Name Four Rainbow
Storage Capacity 600,000 bbls
Production Capacity:
Oil 40,000 BOPD
Liquid 52,000 BLPD
Gas 10 MMSCFD
Ownership 51% YINSON, 49% PREMUDA

*For redeployment opportunity



FPSO Name PTSC Lam Son
Charterer PetroVietnam
Field Block 1-2/97, Vietnam
Storage Capacity 350,000 barrels
Production Capacity:
Oil 18,000 BOPD
Liquid 28,000 BLPD
Water Injection 15,000 BWPD
Gas Compression 47 MMSCFD
Contract Duration 2014 – 2021 (2024)
Ownership 51% PTSC, 49% YINSON



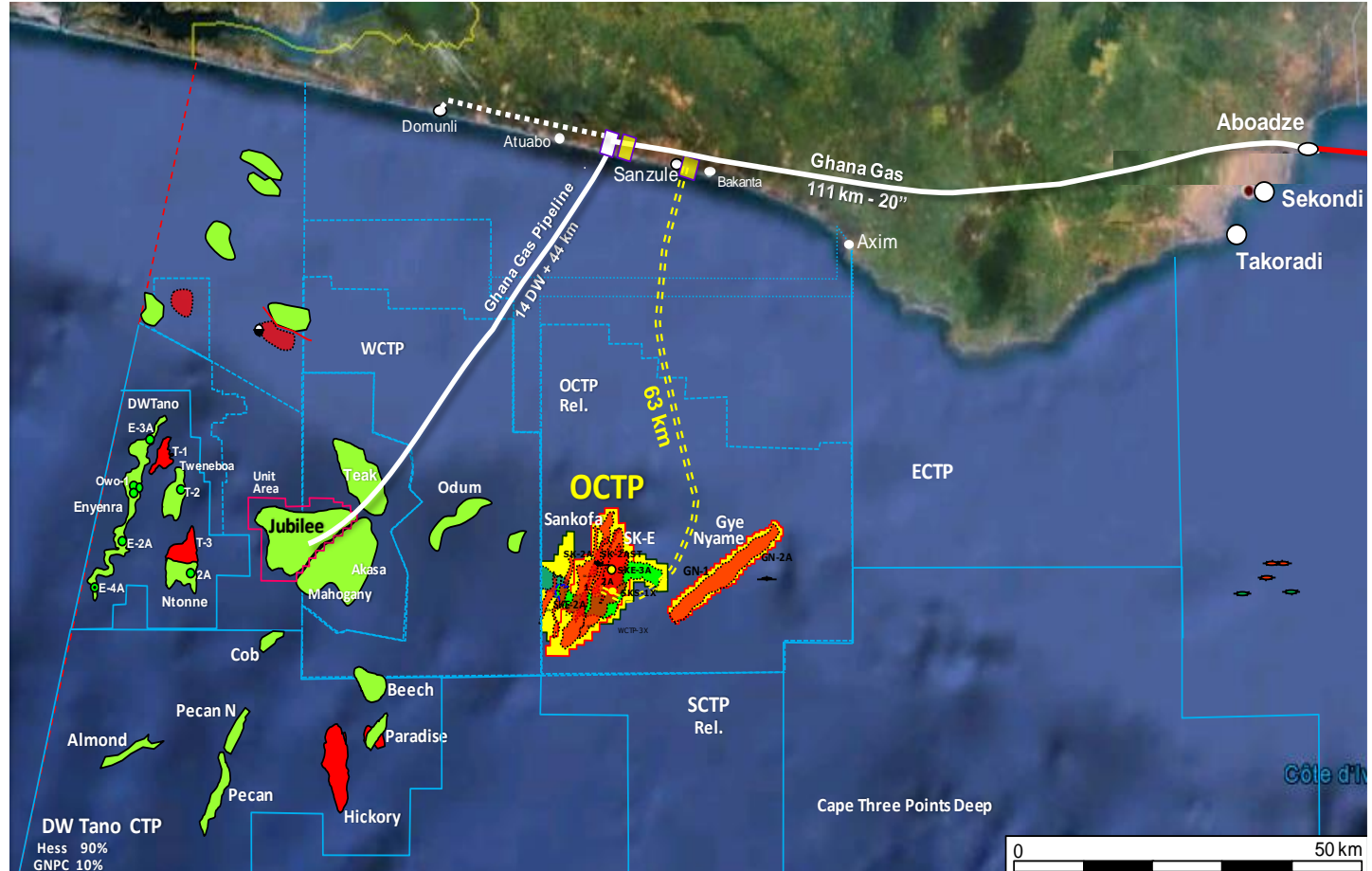
FPSO Name FPSO John Agyekum Kufuor
Charterer ENI
Field OCTP Block, Ghana
Storage Capacity 1.4 million barrels
Production Capacity:
Oil 58,000 BOPD
Liquid 75,000 BLPD
Water Injection 55,000 BWPD
Gas Injection 165 MMSCFD
Gas Export 210 MMSCFD
Contract Duration 2017 – 2032 (2037)
Ownership 100% YINSON



Yinson Production and Eni's OCTP Project

Yinson Production Pte Ltd (YP) is developing the Offshore Cape Three Points (OCTP) field, converting a double hull Very Large Crude Carrier (VLCC) oil tanker to a Floating Production Storage and Offloading (FPSO) to be located offshore of the Western Region of Ghana.

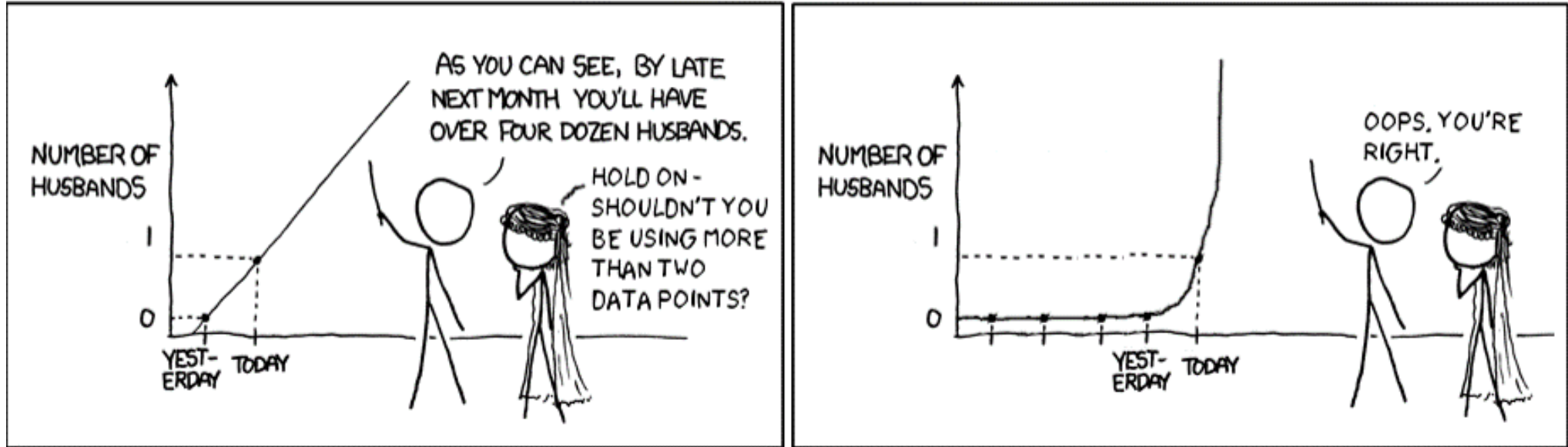
The OCTP block is located in approximately 900m of water depth and about 60km from the coast.



https://www.youtube.com/watch?v=1mxC1_1B6cM

Extrapolating experiences

MY HOBBY: EXTRAPOLATING



Is Experience able to answer all questions?



Motivation for Lifecycle Dynamic Modelling: Challenges

Code is massive in modern ICSS, Can we test it in advance?

Is the design suitable for all potential transients?

How will the vendor packages (UCPs) interact with the ICSS?

Are equipment protected?



Will the Safety System perform well?

How to fully test the Operating Procedures?

Can we improve the plant's availability?

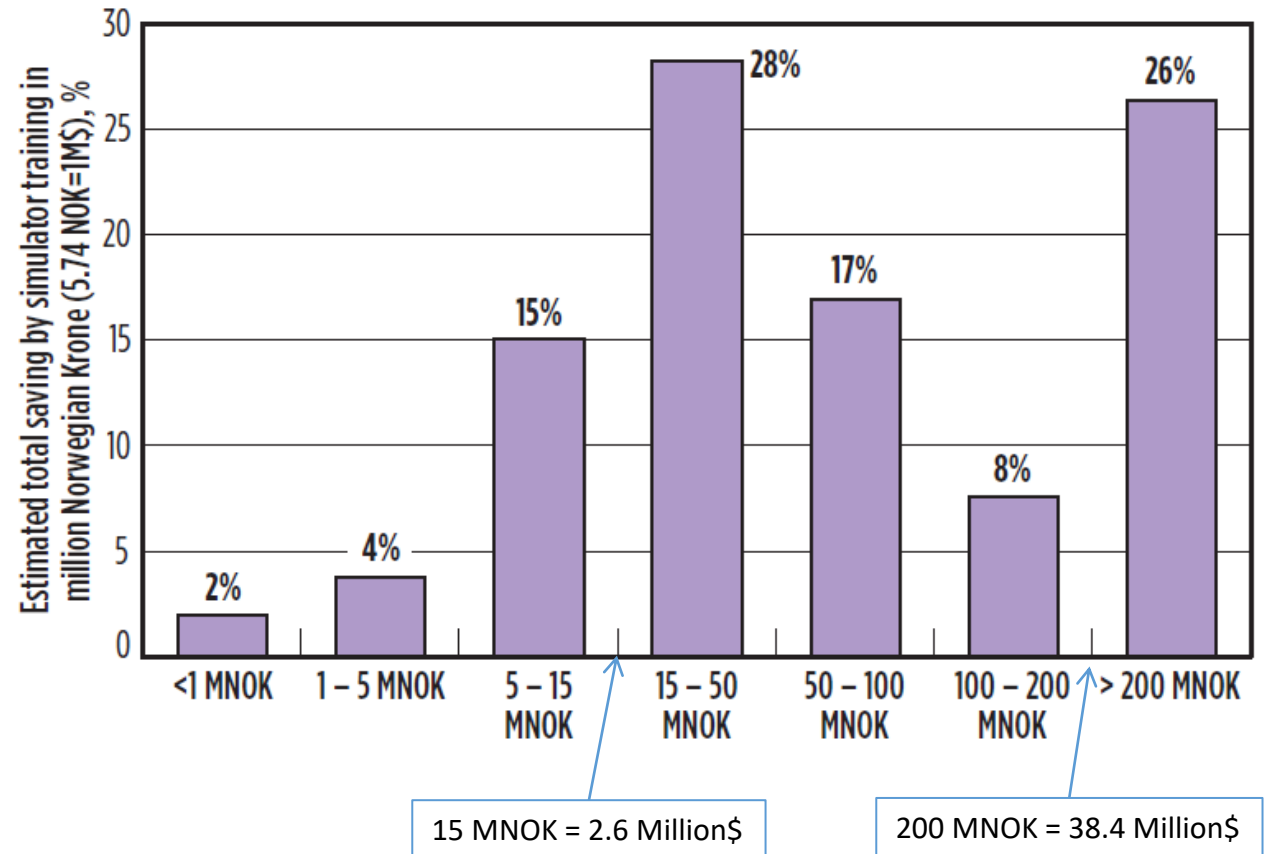
How to effectively train experienced CRO's in advance?

How to safely train inexperienced operators?

OTS Value Survey

- Increased Safety
- Minimize incidents (28% due to human error)
- Shortening start-up: around 10-20 days
- Reducing unplanned shutdowns by 2-3 per year
- Speeding-up planned shutdowns/start-ups by 2-3 days per year
- Increased production by 1-2%
- Flaring episodes minimized

15.3 million\$ average estimated savings due to OTS

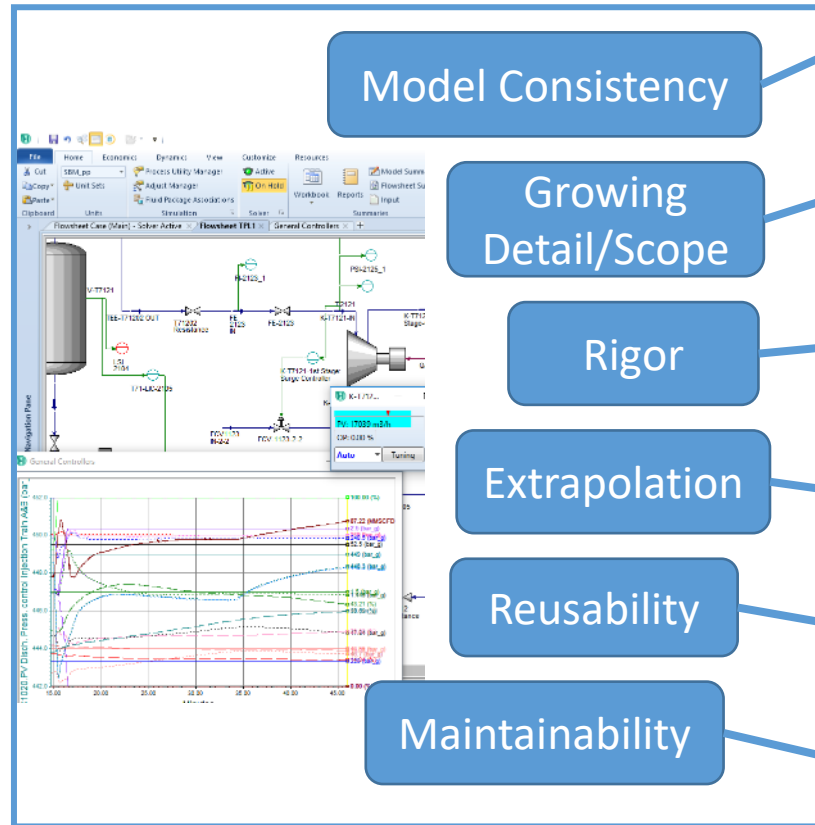


Source: <http://hdl.handle.net/10642/1544>

Motivation for Lifecycle Dynamic Modelling: Why Aspen HYSYS?

Yinson conceived the FPSO modelling from a Lifecycle perspective. But, what additional value does Aspen HYSYS provide to the Lifecycle?

HYSYS LIFECYCLE PILLARS



Thermo Packages are consistent with the Steady-State Design models. Data is introduced once and the model is used along the phases of the lifecycle.

Detailed Equipment data is available and refined as the project evolves. Additional process units can be incorporated as needed in the application.

CRO's will expect realistic process responses. This is the key to replicate/verify/improve operating procedures, pre-tune controllers and define alarms limits.

Extrapolate process conditions far from nominal. Model will help to determine the settings to maximize production, reduce flaring and improve its controls.

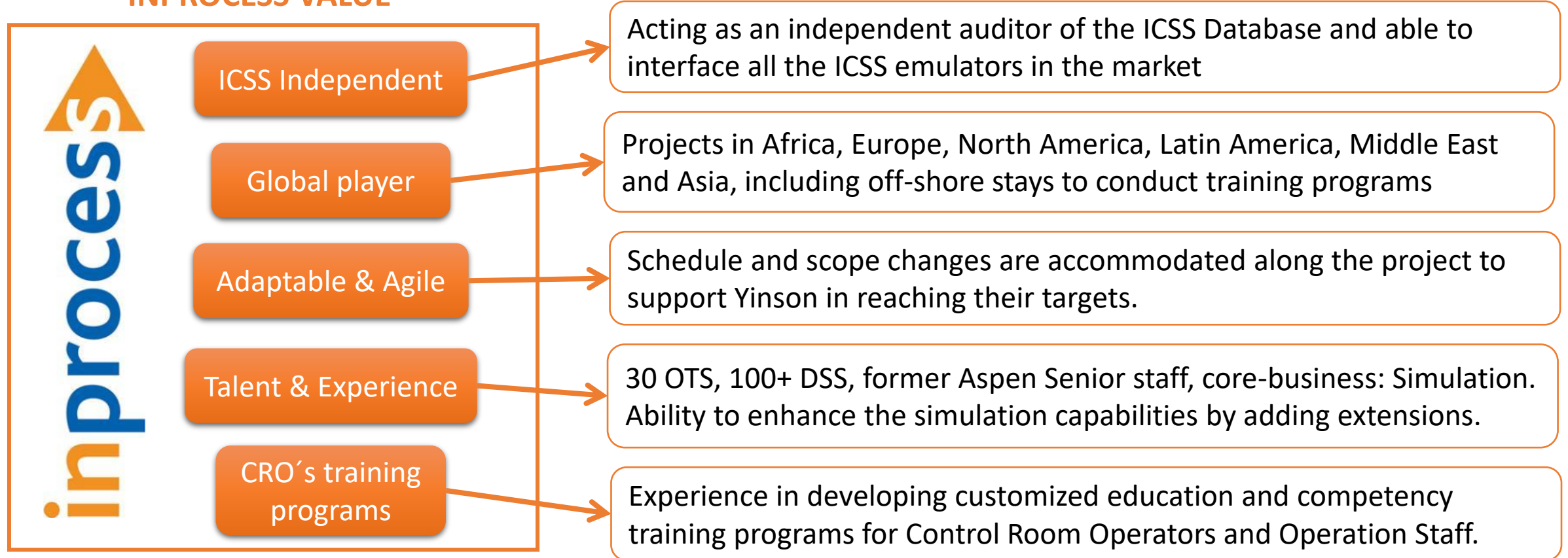
The dynamic model can be re-used with minor modifications for other purposes

Model update workflow is defined to keep the model alive and synchronized with the process, control and procedure changes.

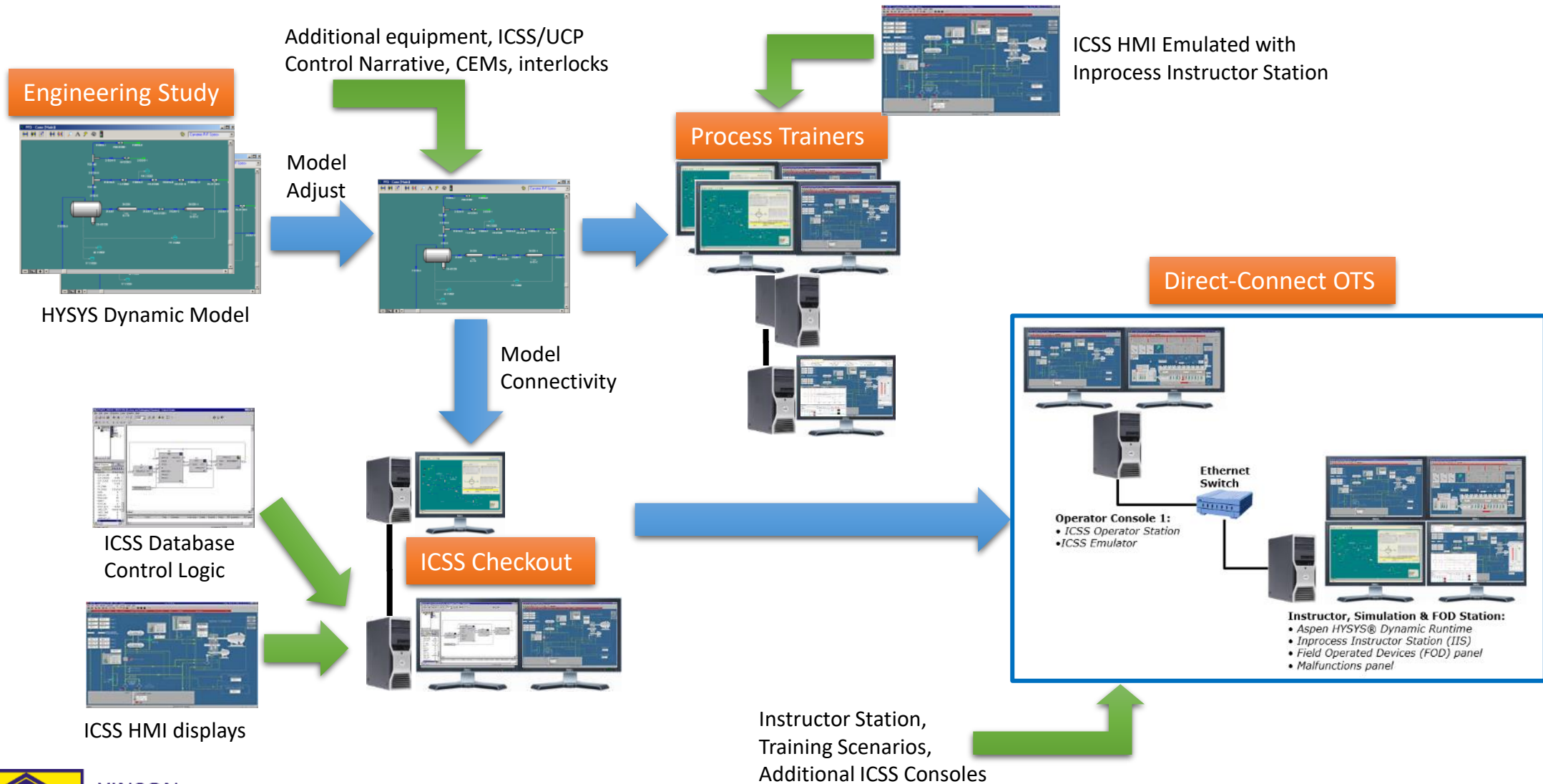
Motivation for Lifecycle Dynamic Modelling: Why Inprocess?

Yinson chose Inprocess as the company to fully exploit the HYSYS Lifecycle Dynamic Modelling envisioned for the OCTP project.

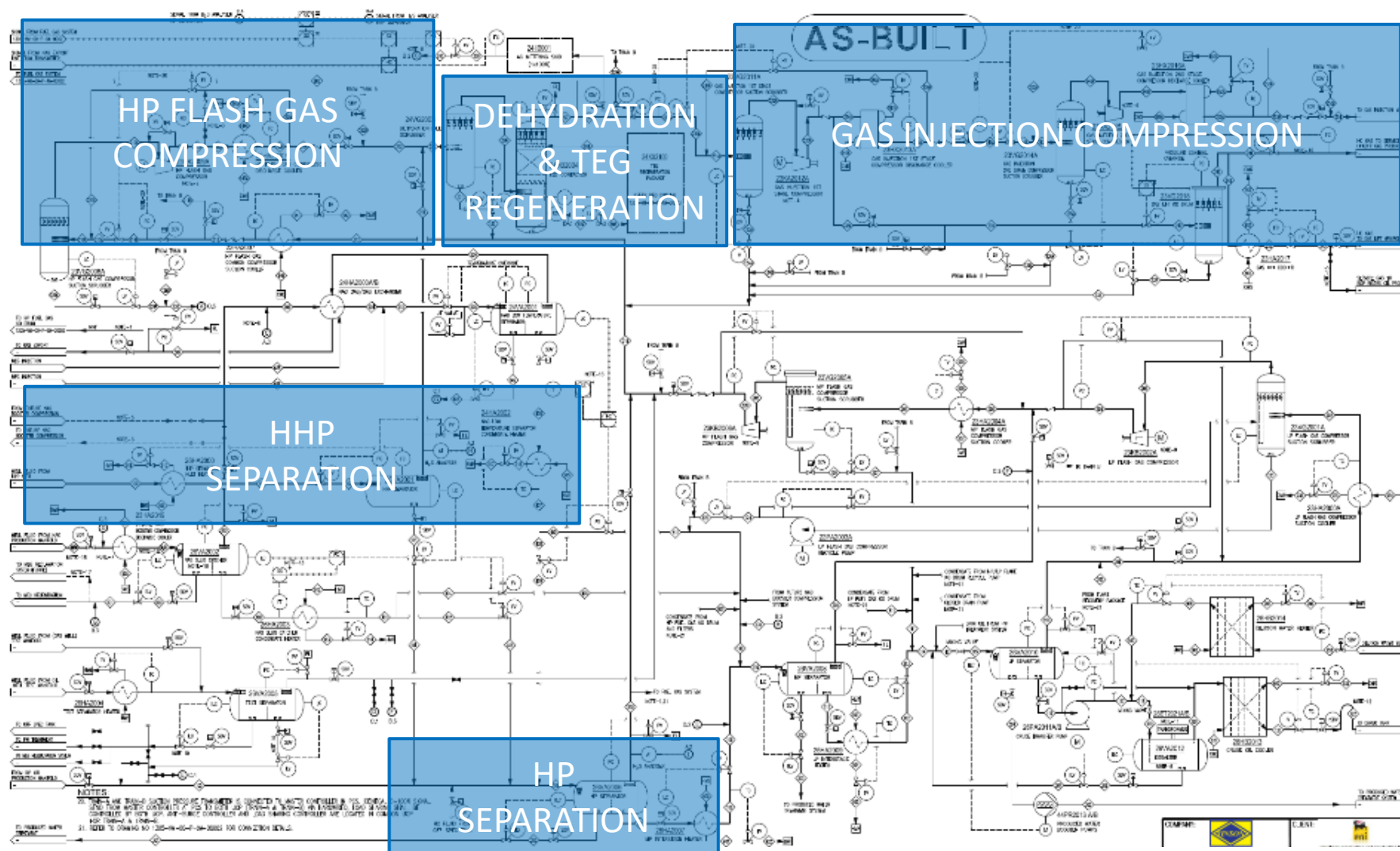
INPROCESS VALUE



HYSYS Lifecycle Dynamic Modelling for the OCTP FPSO

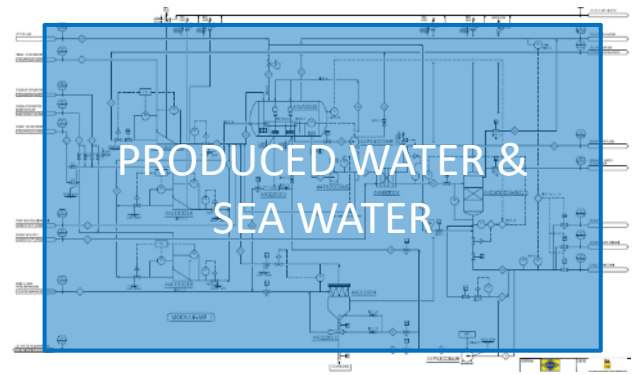


Phase 1: Process Design & Control Validation, DSS model scope



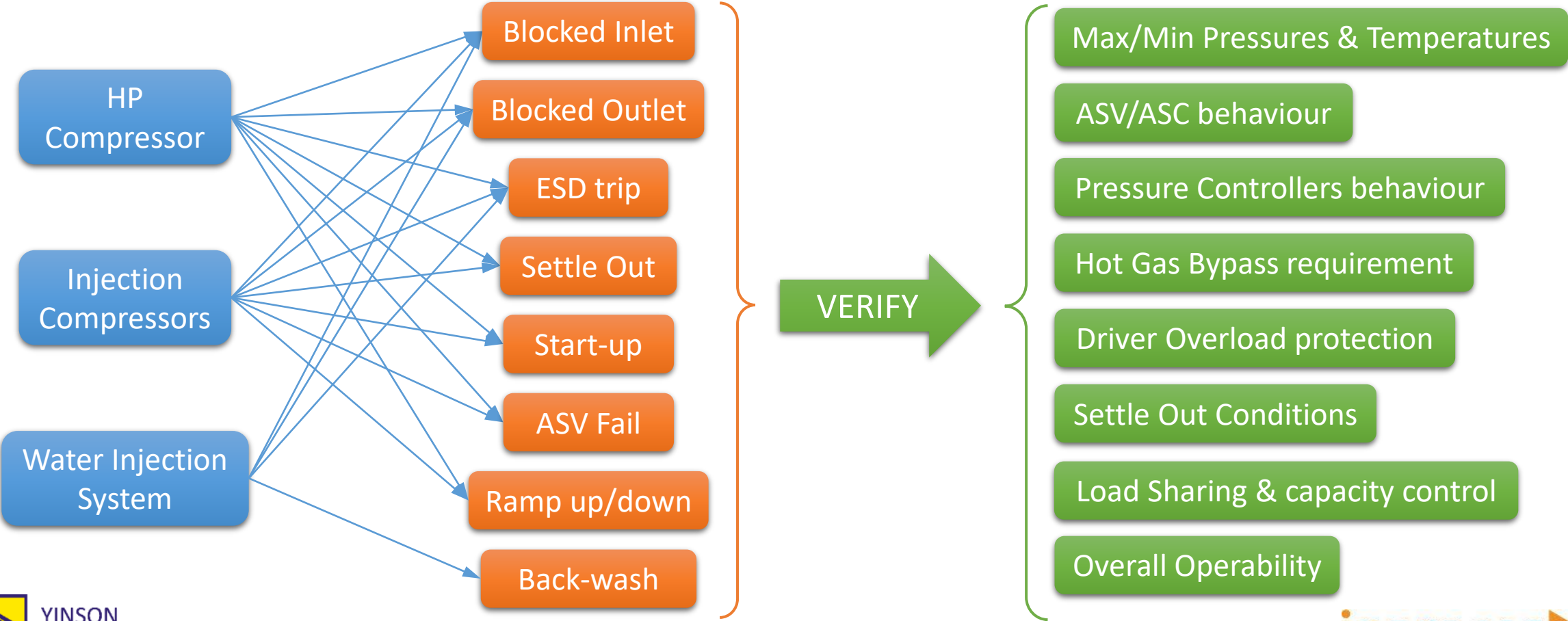
DSS → 

Blue boxes indicate the areas included in the scope of the Dynamic Simulation Study

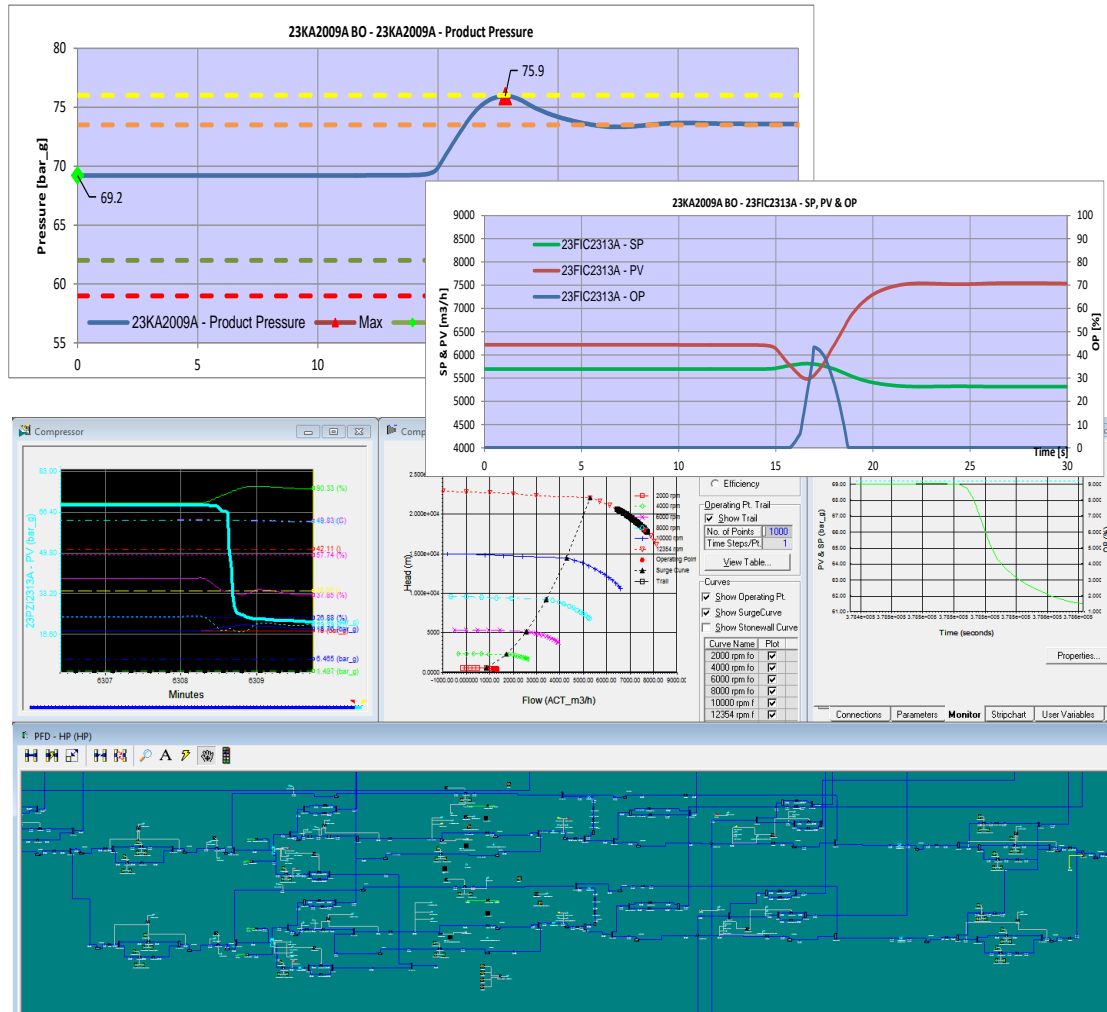


Phase 1: Process Design & Control Validation → Dynamic Simulation Study

20 dynamic simulation studies were performed during this phase to analyse the plant's transient dynamics, the control logic response, the procedures and the necessity of additional protective equipment



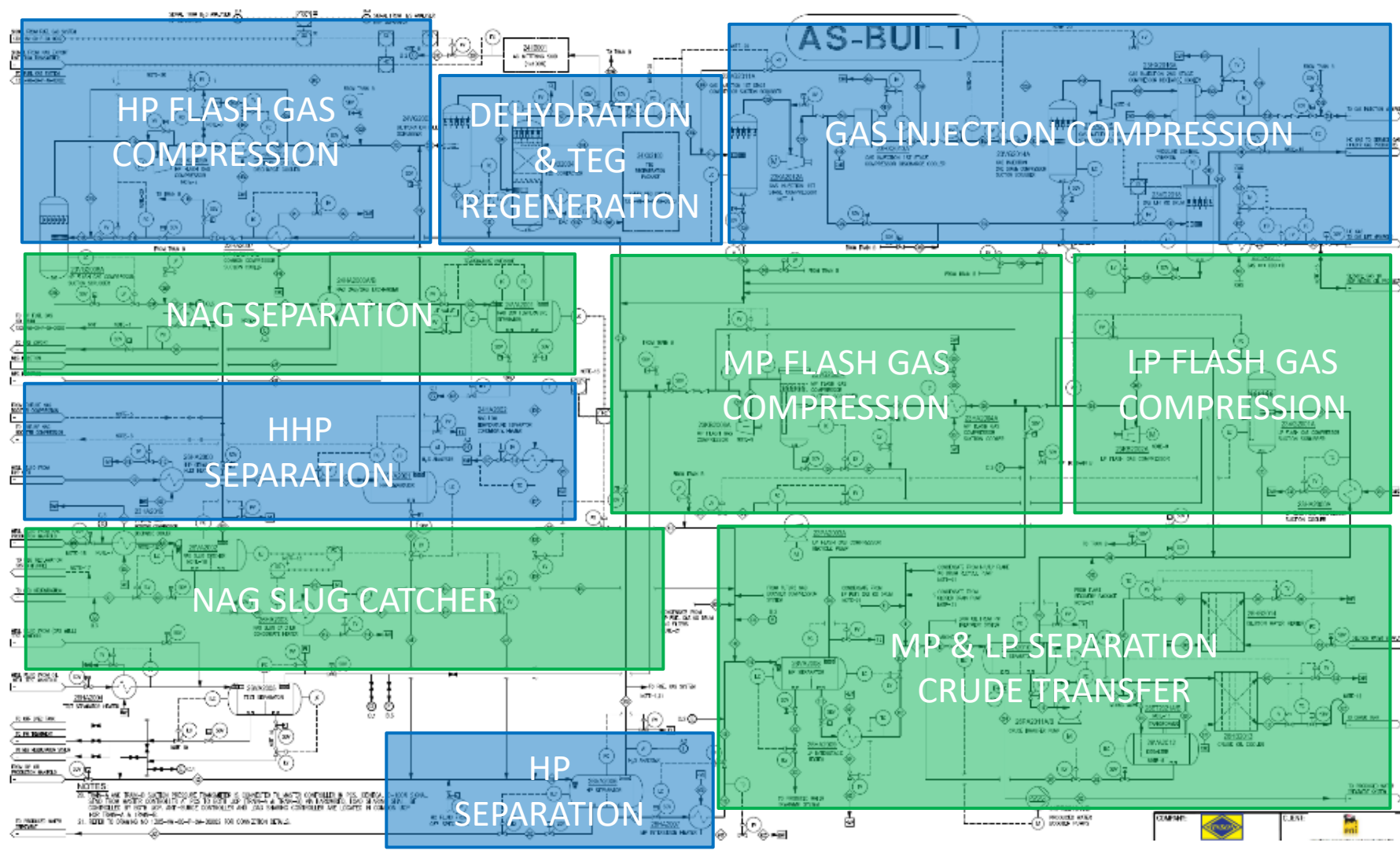
Phase 1: Process Design & Control Validation → Dynamic Simulation Study



Main findings of dynamic analysis:



- Discharge pressure override for throttle valve is required
- Settings of the ASC to avoid certain trip conditions
- Requirements for additional protection in surge scenarios
- No additional torque requirements for start-up after ESD
- Settle out conditions after ESD
- Verification of alarms, trip limits and PSVs setting
- Gain insight of the timing and procedures
- Verification of the 3rd party package procedures

Phase 2: Process Trainer - DSS model scope versus Training model scope



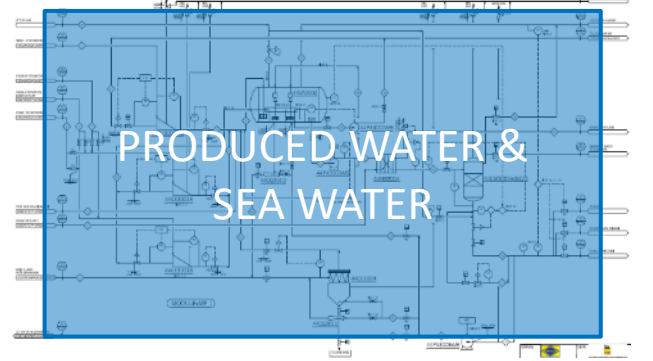
DSS → 

Blue boxes indicate the areas included in the scope of the Dynamic Simulation Study

Training →  + 

Green boxes indicate the areas added to the HYSYS Dynamic model for training

HEATING COOLING MEDIA	MEG REG. SYSTEM	HP & LP FLARE
FG SYSTEM		

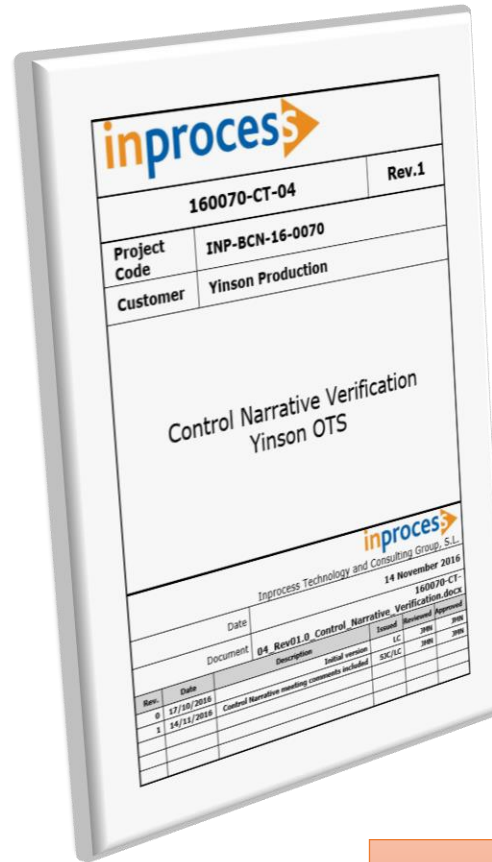


Phase 1/2: Control Narrative Verification

The HYSYS Dynamic model from the DSS was expanded with new units, the latest control logic implemented and the UCP sequences from the compressor packages.

The model was used to verify the Control Narrative Specifications:

- Control interactions with UCP
- Normal operation
- During non-design conditions
- During specific procedures
- Understanding the limits of the system
- Alarm & Trip limits
- Controller pre-setting
- Verify equipment protection

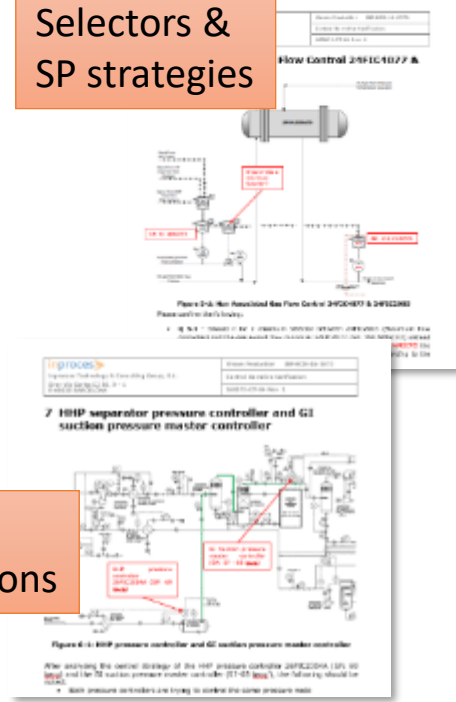


Loops Interactions

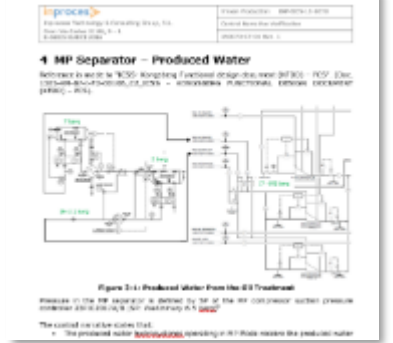
Flare Controller Set Points

ID	Description	Set Point	Reference Procedure	Comments
24P02004	HP Separator Controller	71 barg		HP separator suction master pressure controller setpoint is set to 71 barg on the HP Separator flow controller (24P02004) and one for protection in case of high pressure (24P02004).
24P02005	HP Separator Controller	71 barg		HP separator suction master pressure controller setpoint is set to 71 barg on the HP Separator flow controller (24P02005) and one for protection in case of high pressure (24P02005).

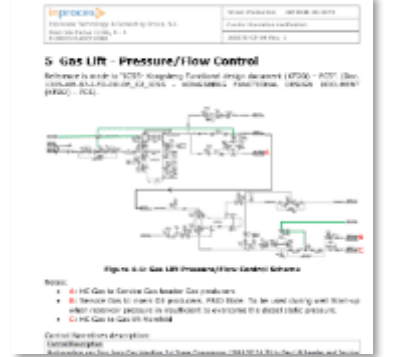
Selectors & SP strategies



Instrument Ranges & Trip Settings



Calculations & Override Controllers



Phase 2: Procedures Verification

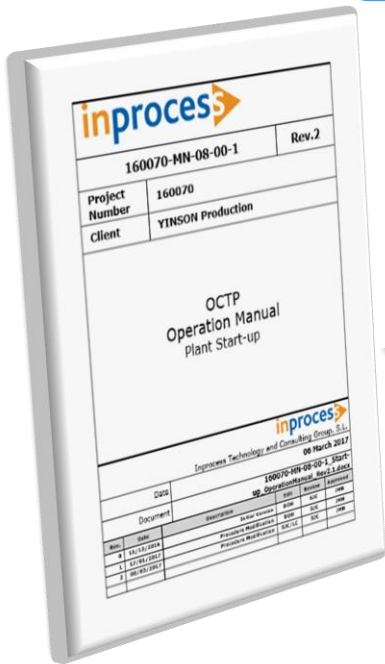
Early verification of Operating Procedures with timing and transitions conditions

Scope:

- Individual Units
- Overall Start-up process

Combining Expertise's:

Mix of experienced Engineers / Operators know-how with realistic response of Process Trainer

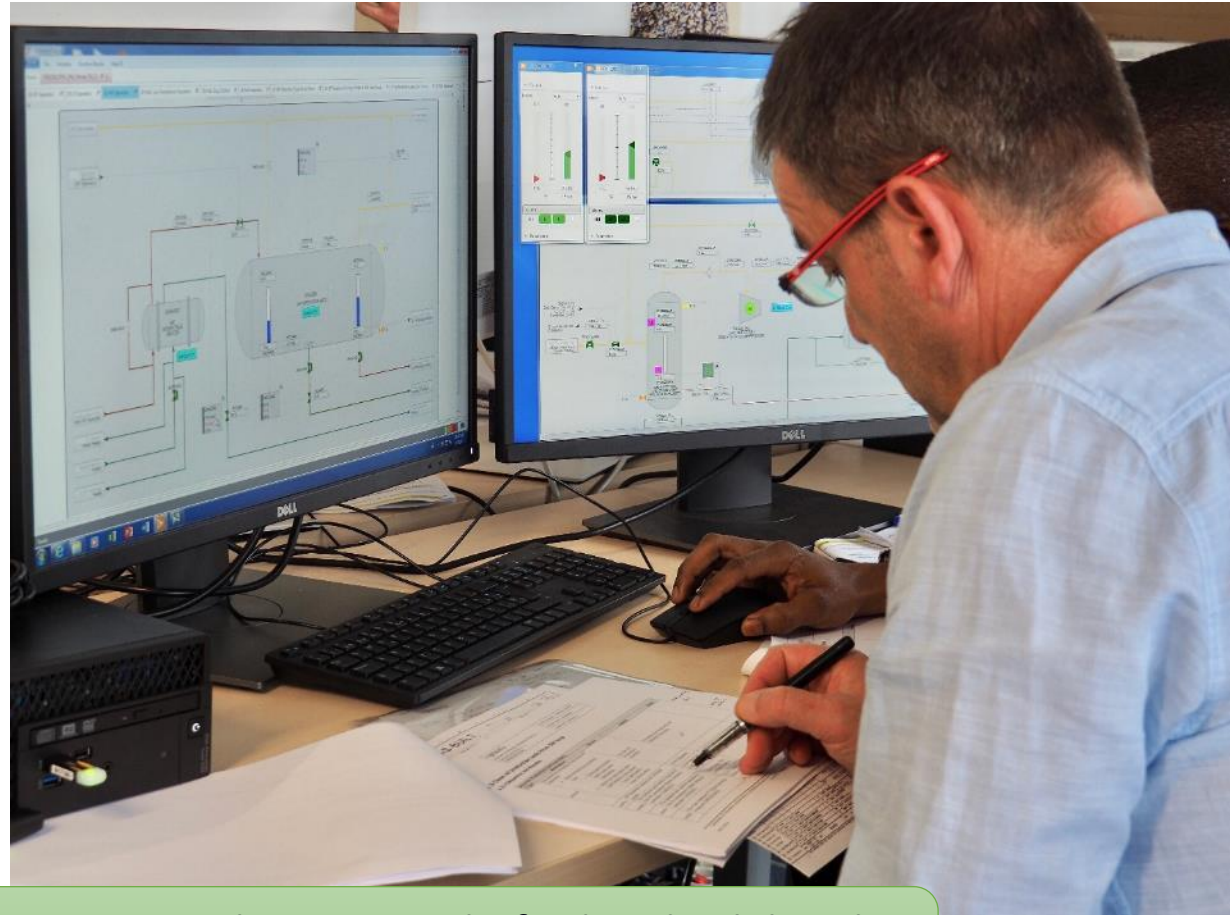


3.1 Summary of Operation Procedures

Reference is made to Operational Procedure for Plant Start-up (MS-OP-KB-50xxx) for a description of the plant start-up. The sequence given in the start-up of the plant via the simulator is equal to the sequence described herein.

Table 3-1 – Operational Procedures

No	Operational Procedure Simulator	Related Operational Procedure	
		Doc. No.	Description
1.	Start-up of HP & LP Flare Drums (Flare system)	MS-OP-KB-50xxx	HP and LP Flare Tip Start-up
		MS-OP-KB-50xxx	Online Replacement of Rupture Discs 43R02001/52 at LP Flare Line
2.	Start-up of Cooling Medium system	MS-OP-KB-50xxx	Online Replacement of Rupture Discs 43R02001/52 at LP Flare Line
		MS-OP-KB-50496	Lining up New Consumers to Heating Medium System
3.	Start-up of Heating Medium	MS-OP-KB-50497	First Start-up of Waste Heat Recovery



Operating Procedures were drafted and validated in a close interaction between Yinson and Inprocess

Phase 2: Process Trainer - Early CRO's Training

Using the *Inprocess Instructor Station* software, an HMI layer was added on top of the HYSYS model using the same displays of the ICSS control room.

Early CRO's and Supervisor Training

Knowledge Transfer

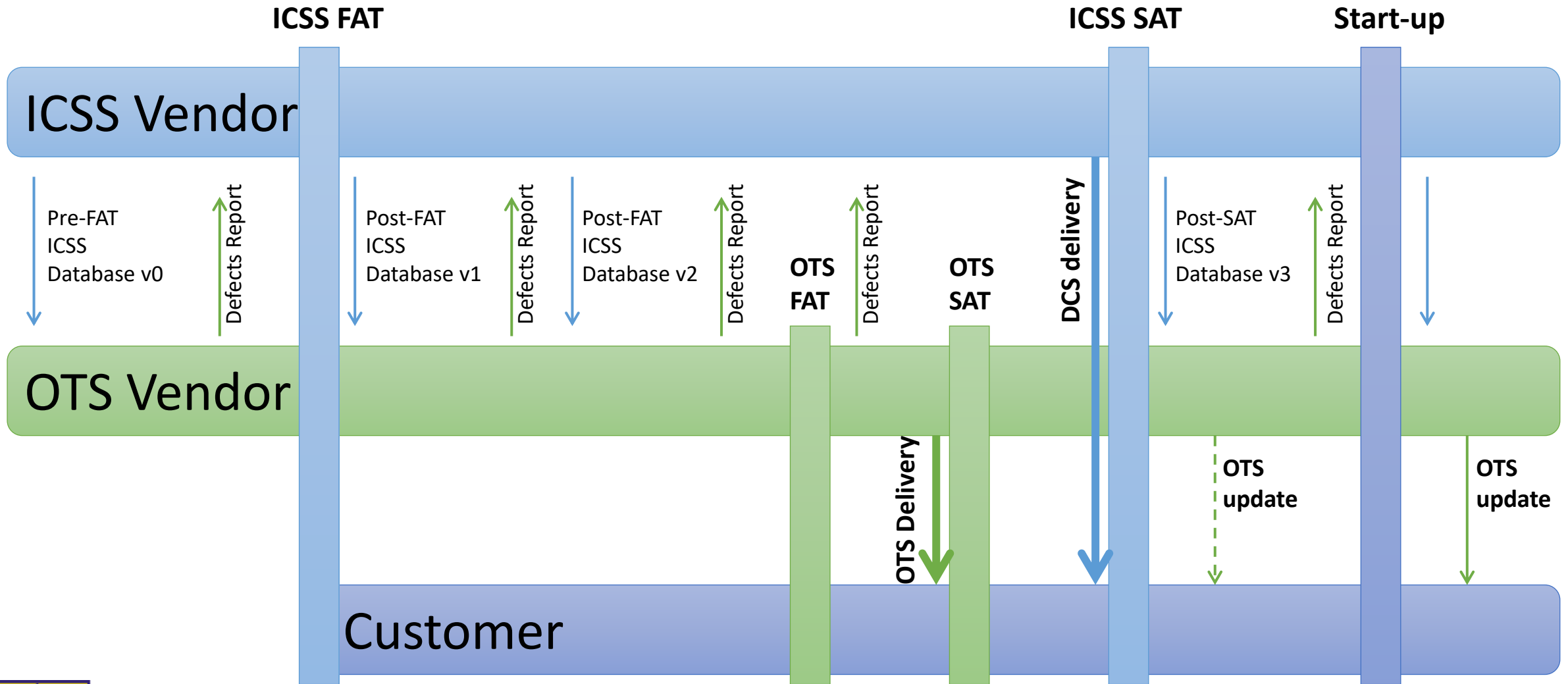
- Control Interactions and Issues
- Limits of the system

Training Scope

- ICSS displays familiarization and operability verification
- Start-up / Shutdown Procedures
- Trip scenarios
- Disturbances and Malfunctions



Phase 3: ICSS Database Checkout



Phase 3: ICSS Database Checkout

	STANDARD ICSS FAT	ICSS FAT with HYSYS
Hardware	Actual ICSS modules	Standard PCs or laptops
Software	Actual ICSS software	ICSS emulator, Aspen HYSYS Dynamics
Location	At ICSS vendor Facilities	At any location (Inprocess, Customer, EPC, etc)
Timing	When ICSS hardware and I/Os modules are available	As soon as ICSS logic and configuration is available
Testing proceeding	Limited to the I/O signal introduced by hand	Same as commissioning & start-up with real plant
Procedures testing	Limited verification	All procedures and start-up/shutdown sequences
Loop testing	No possible	Full, as in real plant
Alarm verification	Only non-time dependent	Full, as in real plant
SIS verification	Limited, no plant interaction	Full, as in real plant

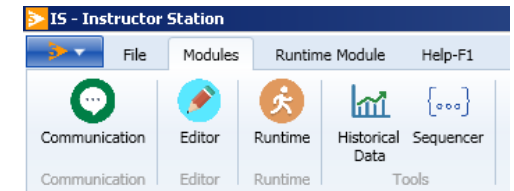
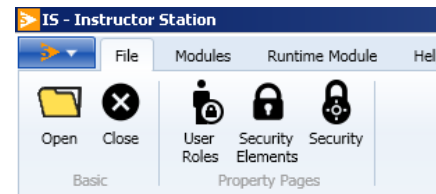
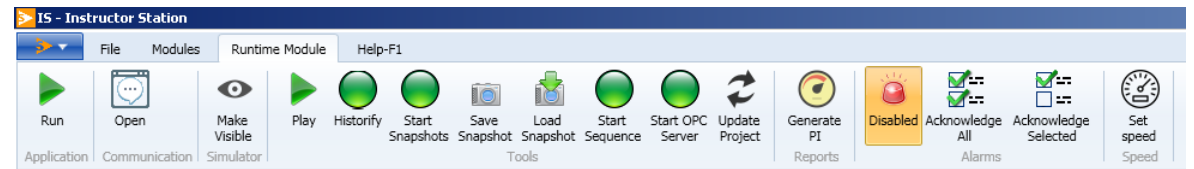
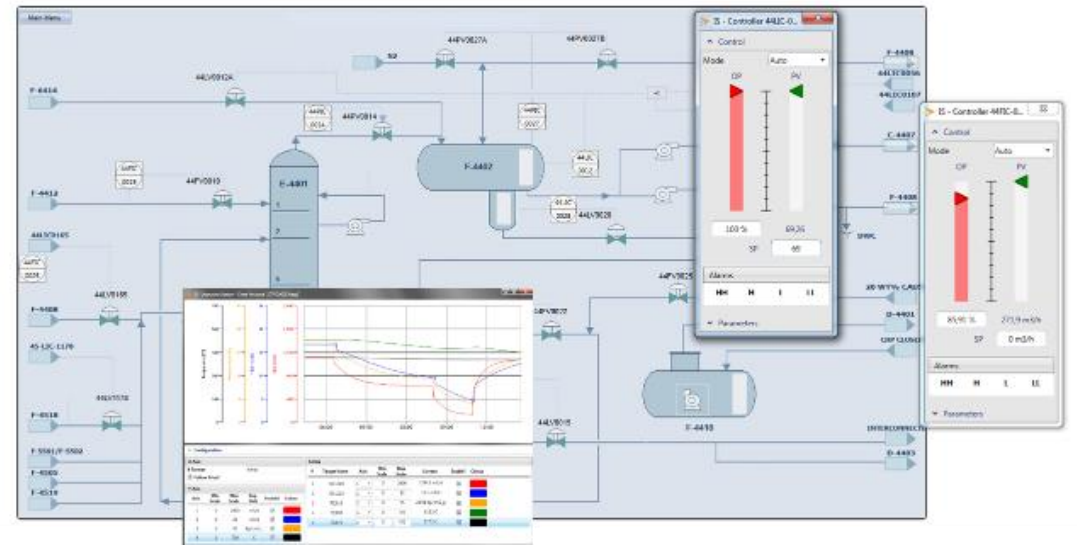
Phase 4: Operator Training System Development - Inprocess Instructor Station

Inprocess Instructor Station (IIS) is the backbone of any Inprocess OTS. IIS is the glue that connects all other data nodes in our OTS solutions.

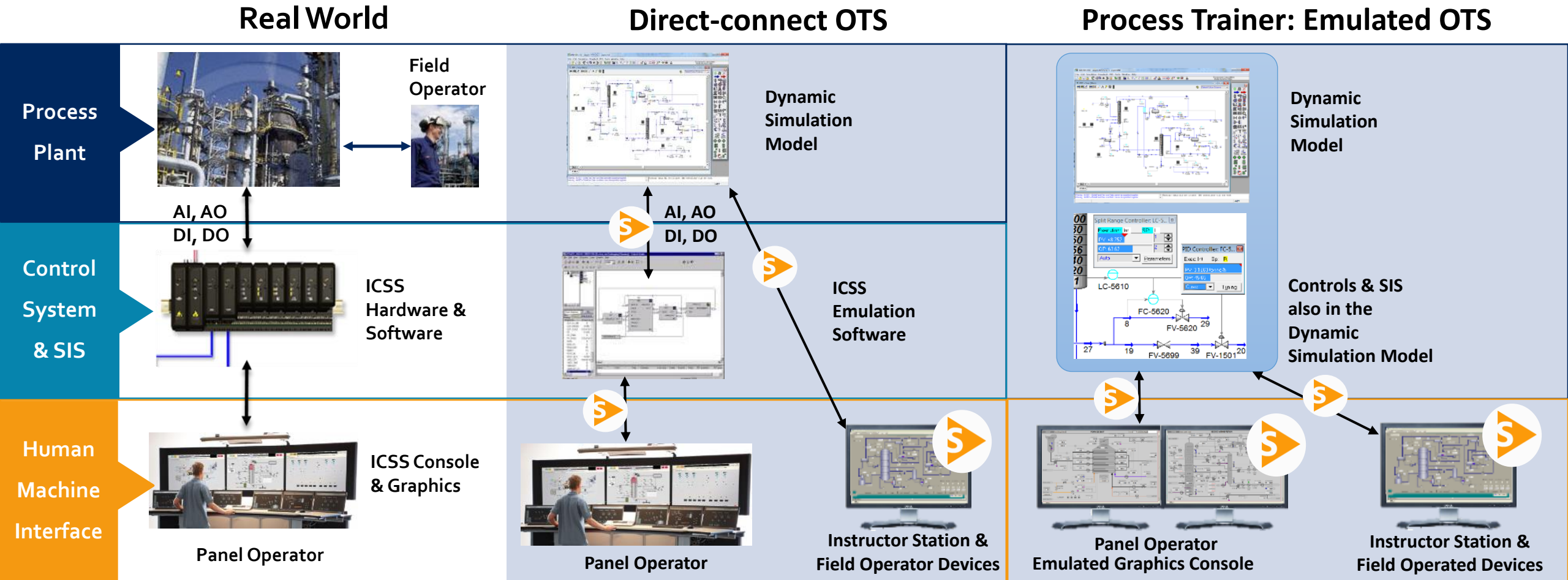
IIS allows to load models, navigate through process displays, make parameter changes, save snapshots, launch scenarios, insert malfunctions, log actions and evaluate operator performance, etc.


Furthermore, the instructor is able to see all the process information available to the operator, as well as certain “key” internal process variables.

It is also used as the Field Operated Devices station.

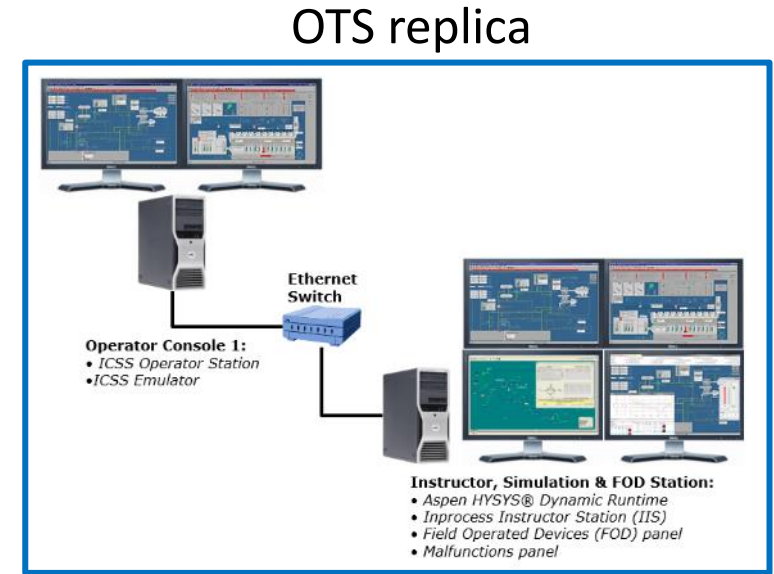
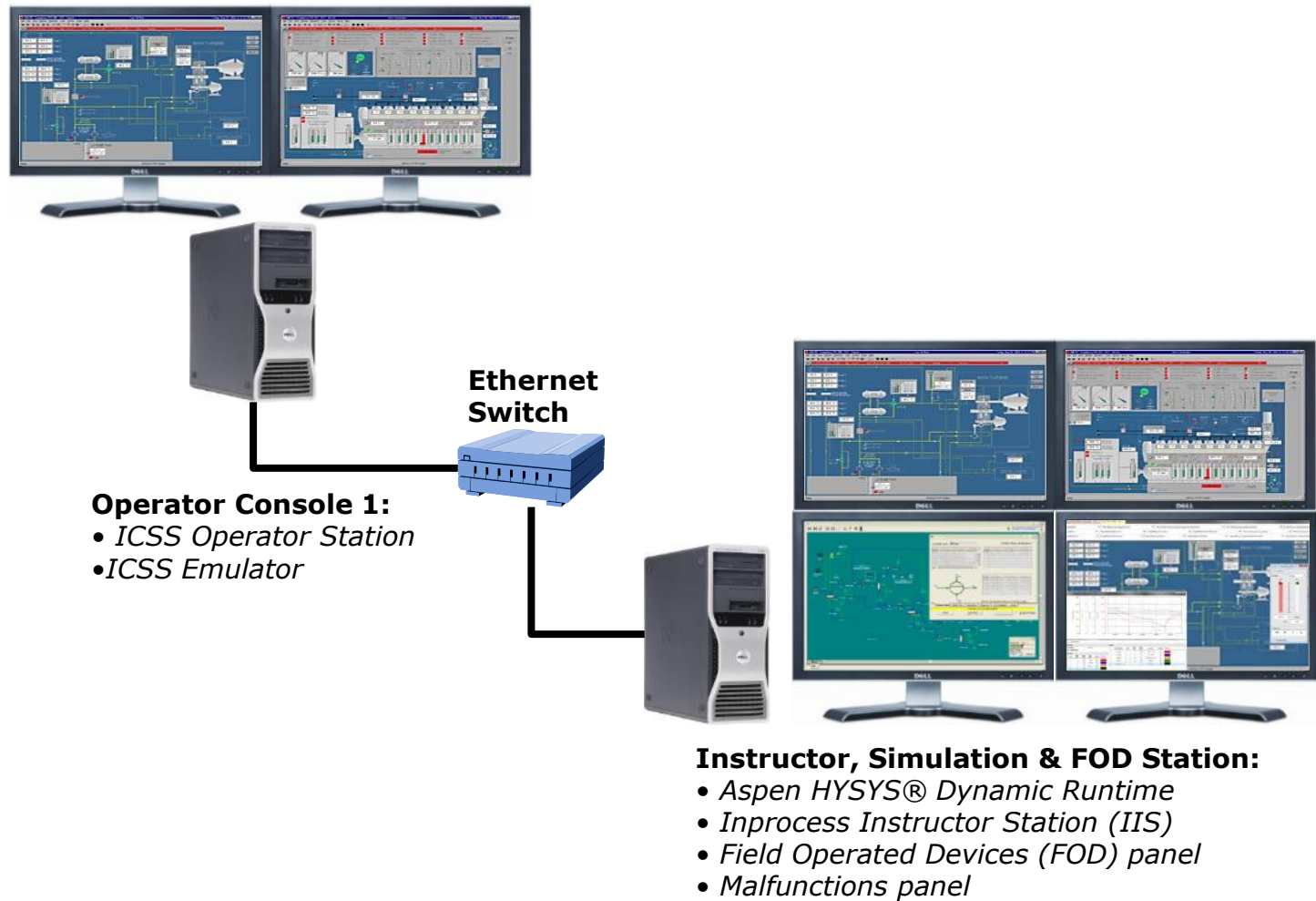


Phase 4: Operator Training System Development



 **Inprocess Instructor Station** connects all these items, and fills some gaps in certain architectures.

Phase 4: Operator Training System Development - Architecture



In addition to the OTS installed in the onshore Yinson Training Center in Ghana, a full replica is also installed at the FPSO

Phase 5: Start-up Support

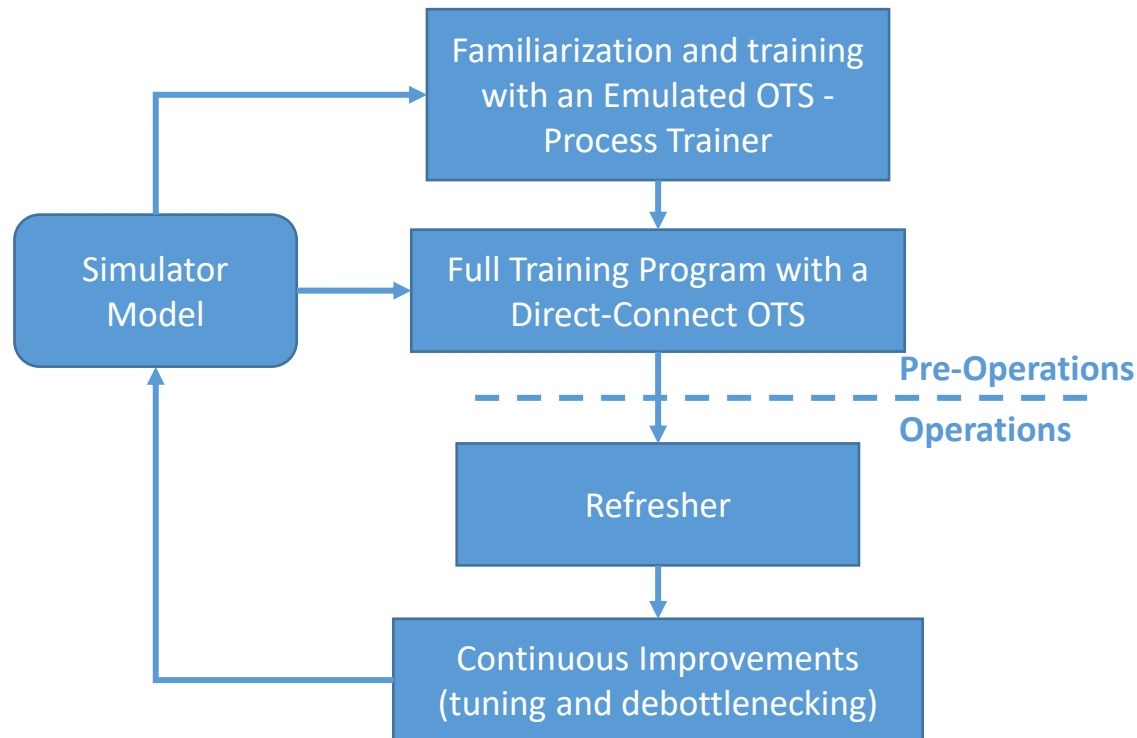
Inprocess project team has been intensively working in the OCTP project during the last 18 months, they accumulate a wide knowledge of the process, control and procedures of the FPSO.

They will be part of the start-up team using the dynamic models and their accumulated knowledge of the process, control, ICSS and procedures.

They will help to troubleshoot potential issues with controllers tuning, alarms setting, start-up procedure, safety system, etc.



Operator Competency Development Program

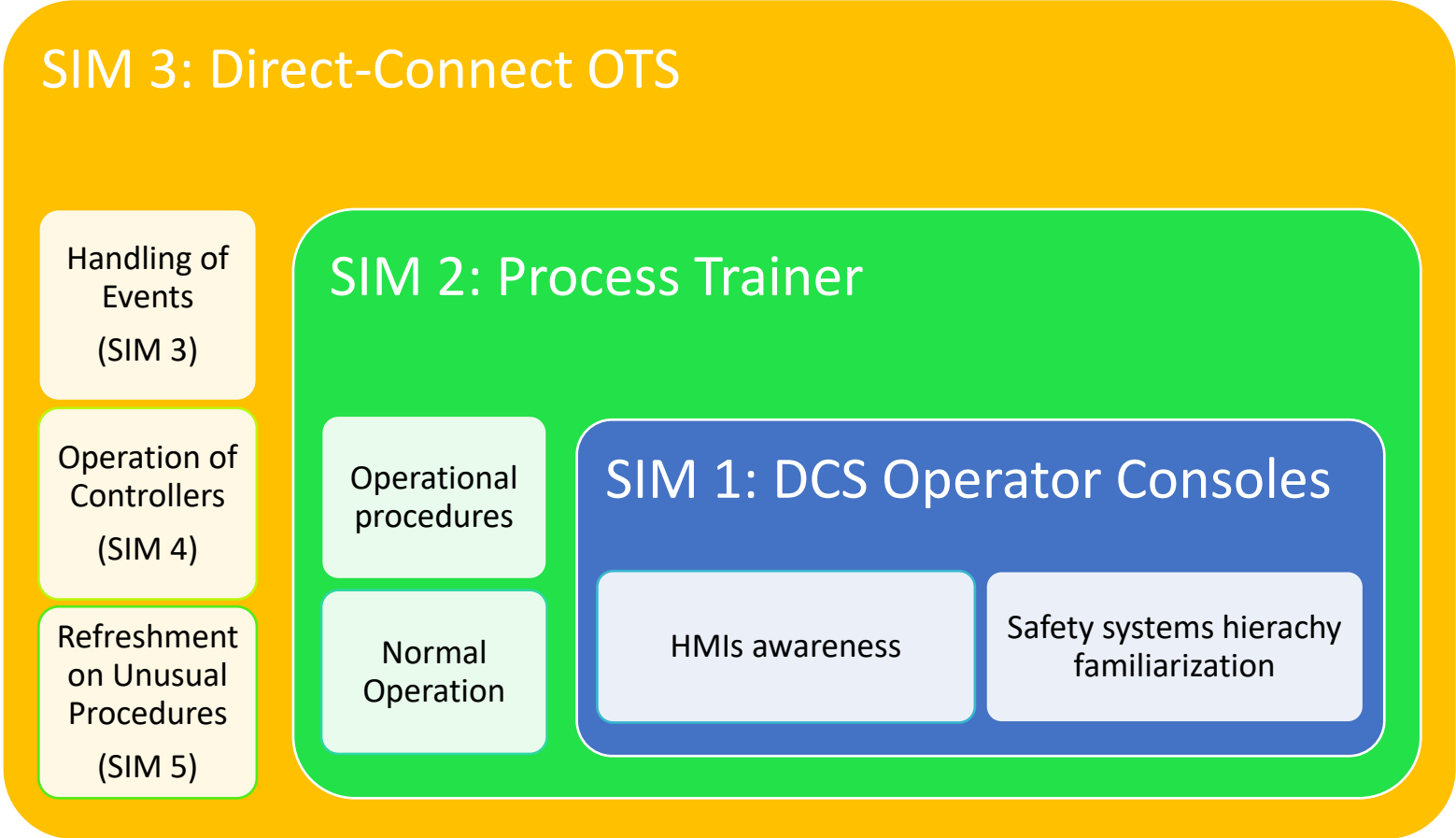


Yinson, in adherence to their Asset Integrity Management, needed an operators competency development plan, based on a high-fidelity simulator model, that should involve the pre-operation, operation and continuous improvements phases of the FPSO:

- The program begins with training sessions to get familiarized with the system and to identify and understand its limitations. The Process Trainer is used to gain process insight and to verify and improve the operating procedures.
- Once the process model is connected to the emulated ICSS, training sessions for all scenarios will commence with the Direct-Connect OTS solution
- Finally, the need for refreshment and continuous improvement during the operations phase leads to continuous updates in the real ICSS and in the OTS

Operator Competency Development Program

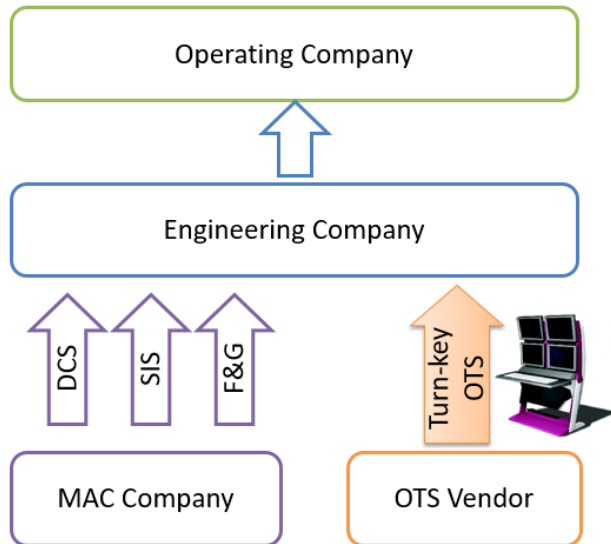
Along three project stages, Yinson will benefit from different project deliverables to develop the skills of the FPSO operators:



Yinson's approach to Lifecycle

In order to fully exploit the HYSYS Dynamic modelling lifecycle, Yinson decided to outsource the development of their OTS to a supplier (Inprocess) who is independent from the ICSS supplier.

FIVE REASONS TO DECOUPLE OTS FROM THE REST OF ASSET AUTOMATION ACTIVITIES



- 1. Fast tracking projects.** By building an early OTS based on dynamic models, you are freed up from waiting until every detail and revision of the plant DCS is complete.
- 2. Safer operations.** By basing the OTS on dynamic process models, more rigorous and comprehensive safety scenarios can be considered, and impacts can be modeled and assessed.
- 3. Operator training as an area of excellence.** By entrusting the development of OTS to dynamic modeling experts, you are involving teams passionate about the topic. You are selecting for excellence rather than just tacking on a must-have to a contractor focused elsewhere.
- 4. Optimizing for cost & responsiveness.** By decoupling the OTS, the owner is encouraging competition, and more likely to get the most responsive and best price / performance solution.
- 5. Agility.** A dynamic modeling team, not dependent on DCS design and delivery, can be extremely responsive to changes in operating objectives, staffing plans, regulations, etc.

Extract from Ron Beck blog: <https://www.aspentech.com/Design-Optimization/A-Dynamic-Model--The-Essential-Accompanyist-to-the-Project-Conductor!/>

Conclusions

TASKS

BENEFITS

HYSYS Lifecycle Dynamic modelling

Engineering Study

Process Trainers

ICSS Checkout

Direct-Connect OTS

Start-up support

Discover engineering design issues (Equipment sizes, Protection Systems, 3rd party packages, ...)

Verify Control Narratives specifications and ICSS ↔ UCP interactions

Verify CEMs and trip logics specifications

Verify Start-up/Shutdown/ESD Procedures

Pre-tune Loops and alarm settings

Check out ICSS implemented code and UCPs

Knowledge Transfer Program - Training of Operators with Process Trainer/OTS

Engineering support for troubleshooting

Reduce start-up date delays

Shorten start-up

Minimize incidents

Reduce unplanned shutdowns

Minimize flaring

Improve plant reliability

Improve safety

Q&A



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