

Holistic Process Digital Twins

Benefits of integrating pipeline and top-side process models

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- **Inprocess at a glance**
- **Process Digital Twin**
- **Multi Purpose Dynamic Simulator (MPDS)**
- **Case Study**
 - Project Overview
 - Operation Scenarios Results
 - Comparison
- **Conclusions**



Since 2006 helping the processing industries in solving design and operational issues by applying process simulation

inprocess

our **core business** is Process Simulation

enthusiastic about **sharing our knowledge** with our clients

technology **neutral** (process simulator or control system)

Inprocess Solutions & Services



Operations Insights and optimization



Engineering Studies: De-bottlenecking Flare System, etc.



Operator Training



Engineering Training



2006

est. in Barcelona by domain experts



Projects in 55 countries

worldwide presence



70+

simulation engineers



400+

executed projects



>70

OTS Projects

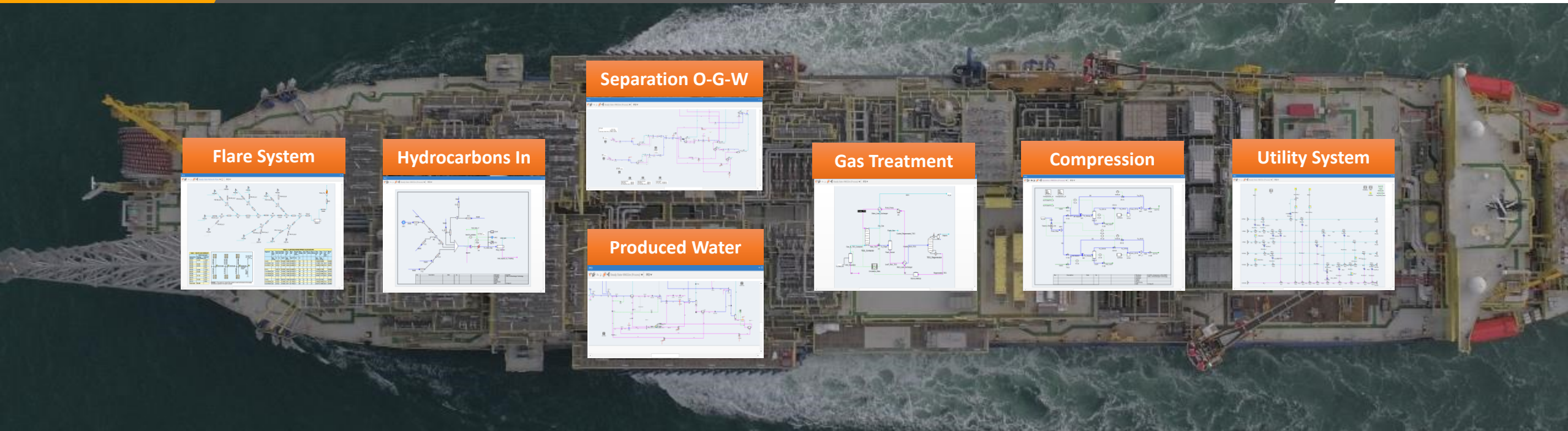


330+

training courses

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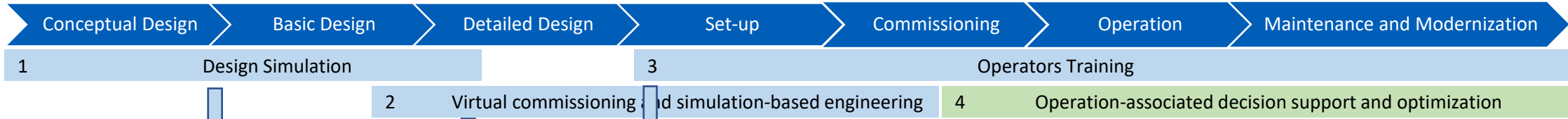


The Process Model is a *first-principles* virtual representation of the plant that contains:

- all the process layout and streams conditions (Compositions, Pressure, Temperature, Flow, etc);
- Selected equipment geometric data (dimensions, elevation, tray sizing, sensor location, etc);
- Selected equipment manufacturer performance data (pump curves, compressor curves, heat exchanger rating data, etc);
- Selected actuated valves (valve pressure drop, sizing, characteristic, etc); and
- Selected control and instrumentation (control loops, PID algorithms, instrument ranges, tuning constants, etc).



Plant lifecycle

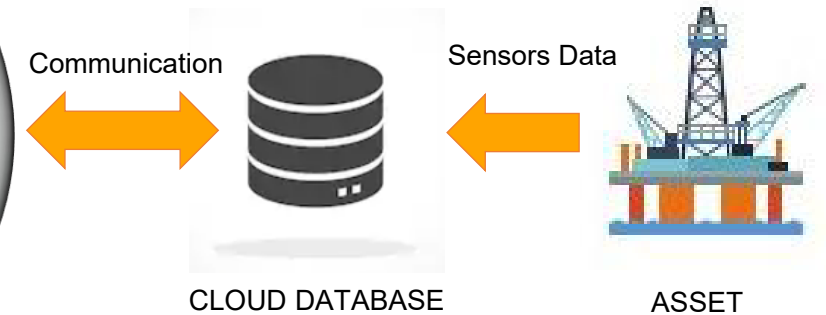
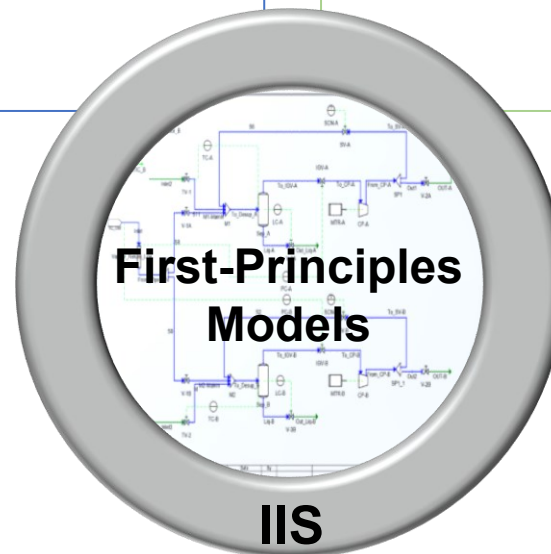


Off-line

- Engineering Design validation
- Control Narrative & Procedures validation
- ICSS validation & tuning
- Operator Training Simulators (OTS)

On-Line

- Equipment Load & Efficiency Monitoring
- Inferentials
- Bad Actors Detection
- Look-ahead & What-if



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Transient Scenarios during Detailed Engineering Phase

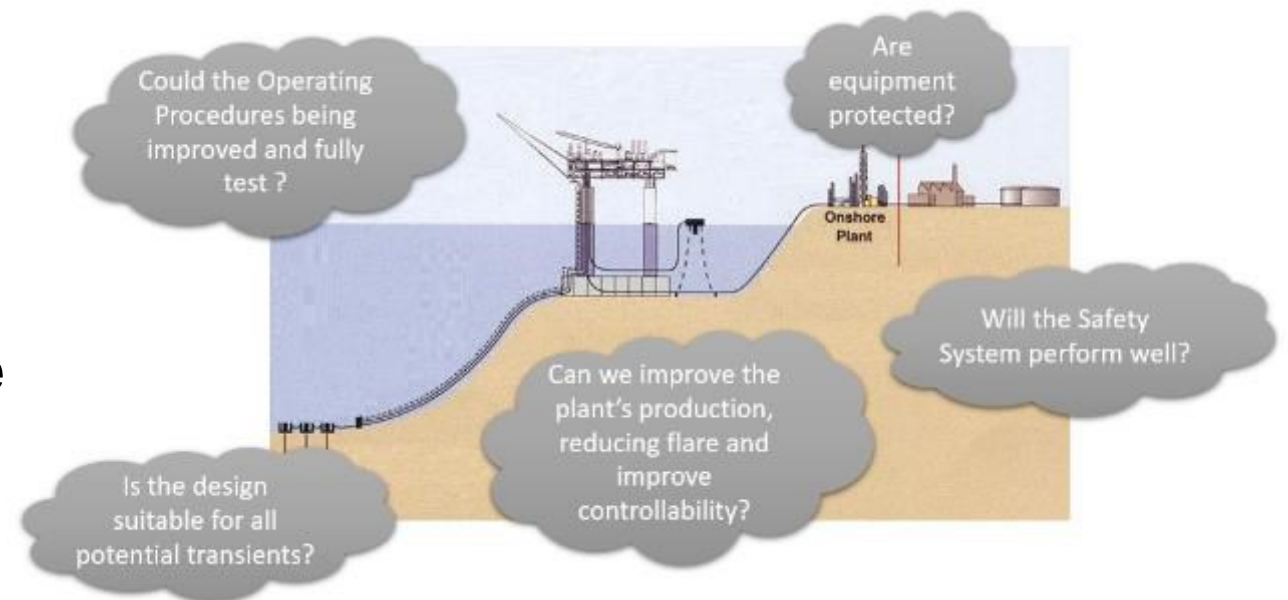
- Emergency Scenarios: Equipment and Instrumentation design check in front of trips, blocked lines, changes in production
- Control Philosophy: Control loops, alarms settings

Start-Up Operations

- Facilities Start-Up, wells management
- Early Production Simulation
- Transition to Normal Production

Daily Operations and Maintenance

- Analysis for future production rates & operational constraints
- Online Process Digital Twin



Process Unit Dyn. Models

Engineering Data
Plant Data
Model from engineering Studies

Analysis of critical units



Additional equipment, ICSS/UCP Control Narrative, CEMs, interlocks

External packages → logic and sequence implementation

Complete Dynamic Model

Control Narrative and Procedure Verification



Process Trainer = Emulated OTS

ICSS HMI Emulated with Inprocess Instructor Station

Early Operator Training

ICSS Database Control Logic

Virtual Commissioning

ICSS HMI displays

PID Control tuning DCS Check-Out



Instructor Station, Training Scenarios, Additional ICSS Consoles VR

Direct Connect OTS

OTS Training OTS Maintenance



Connectivity to Plant Data Base

Online Digital Twin

Define Applications – e.g. hydrates or chemicals monitoring

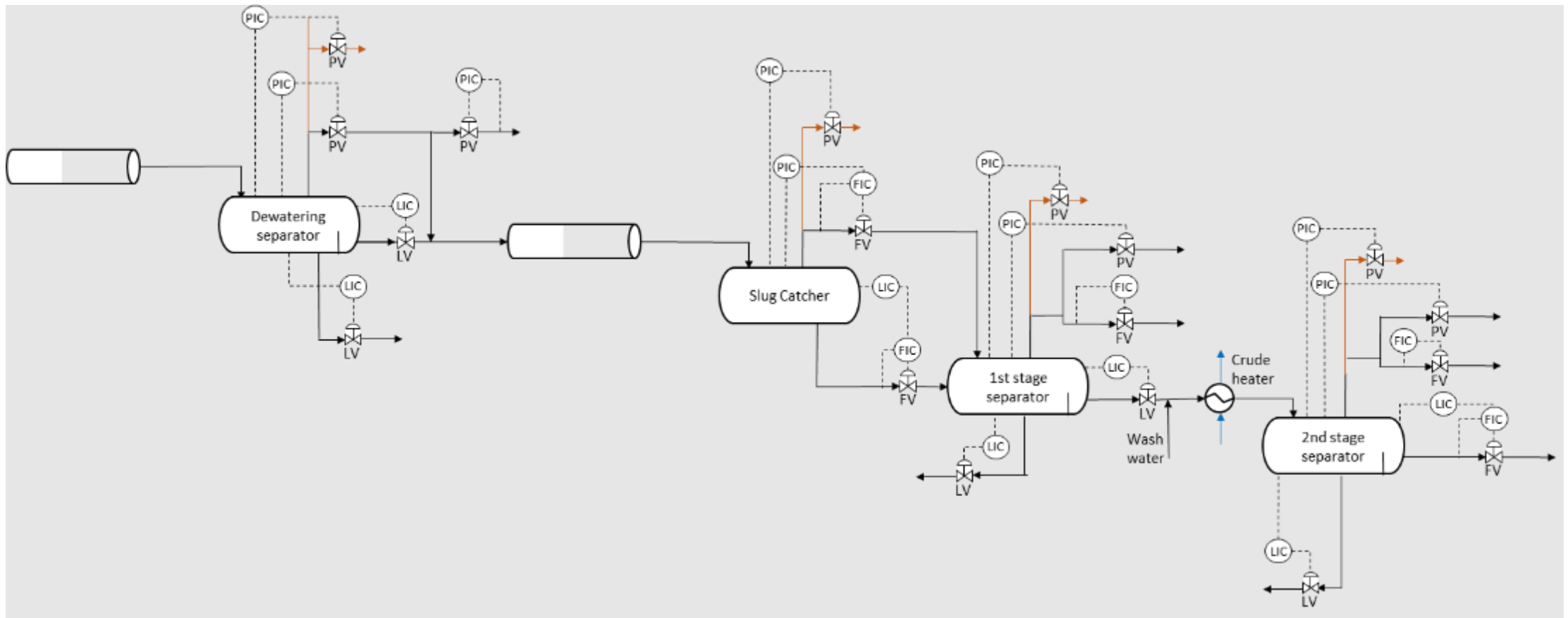
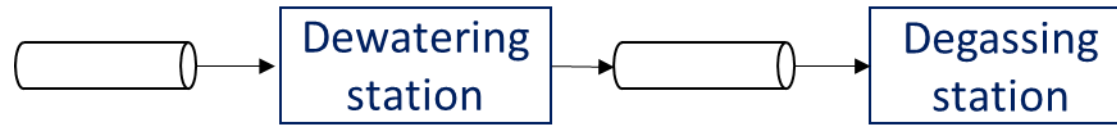
Operational Insights What-if Analysis Bad Actor Detection

Multi Purpose Dynamic Simulator (MPDS) offers continuous value during the project lifecycle:

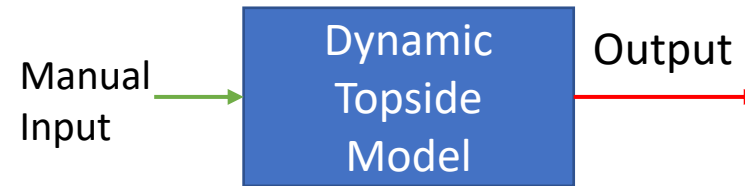
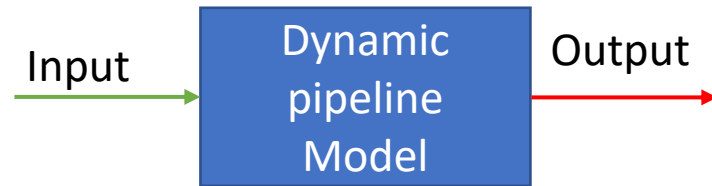
- De-Risking Start-Up through Virtual Commissioning
- Effective Operator training when required (even with DCS delays)
- Process & Control insights during Project Execution
- Resilient Benefits from Simulator investment → Online Process Digital Twin
- Aligned with Digitization Strategy
- Future-proof Investment → >80% of Inprocess OTS are still under Maintenance

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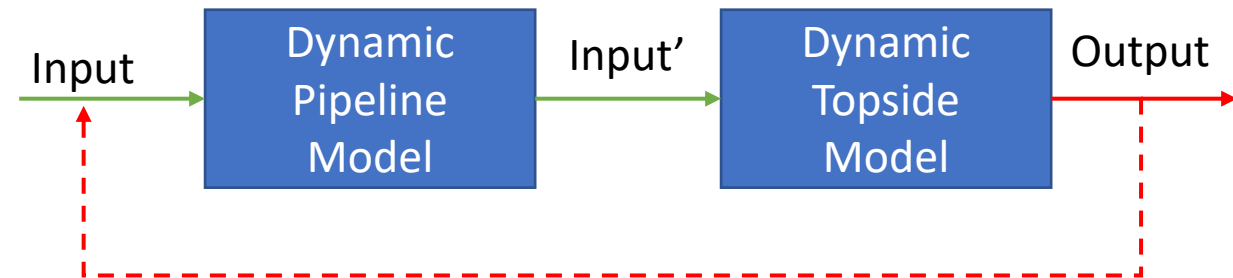




Models not integrated

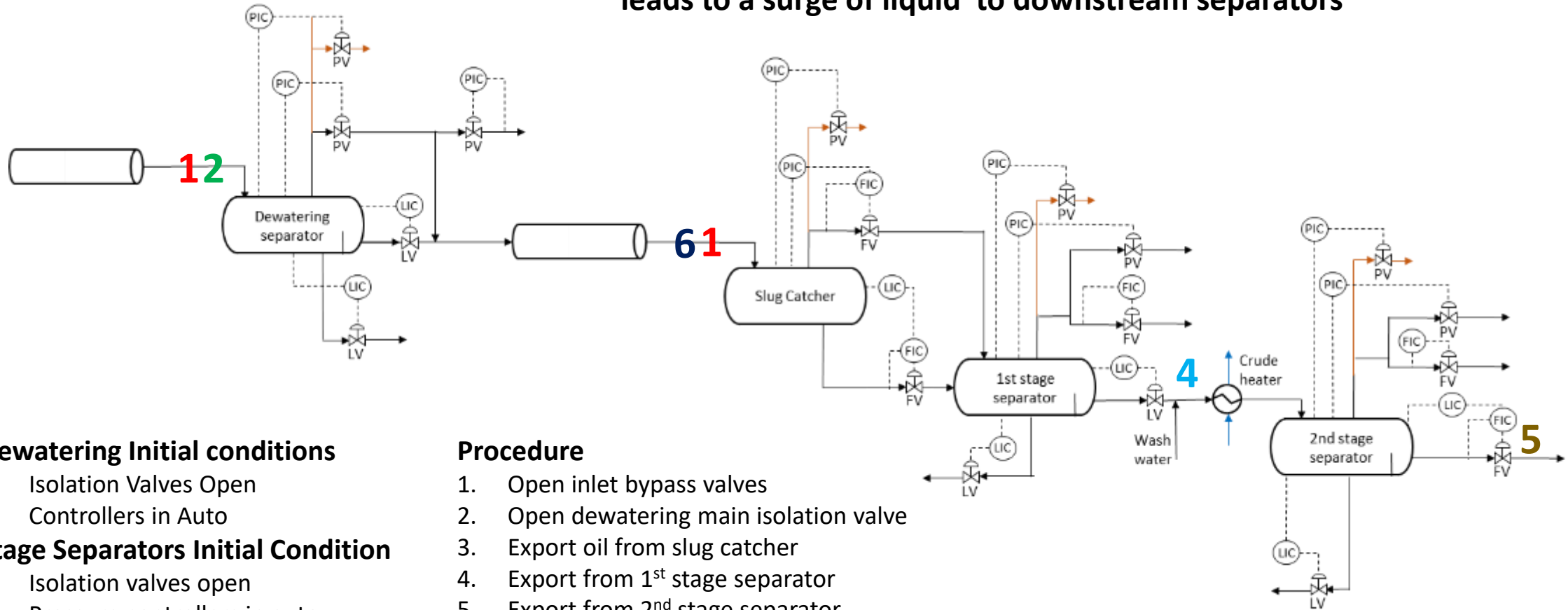


Integrated Models



Objectives

- Ensure trips are avoided during the start-up
- After ESD some liquid remains in the piping. During start-up this leads to a surge of liquid to downstream separators



Dewatering Initial conditions

- ✓ Isolation Valves Open
- ✓ Controllers in Auto

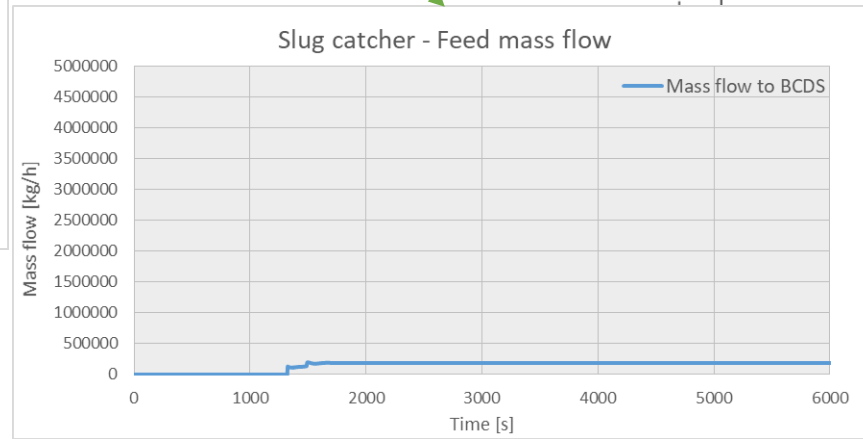
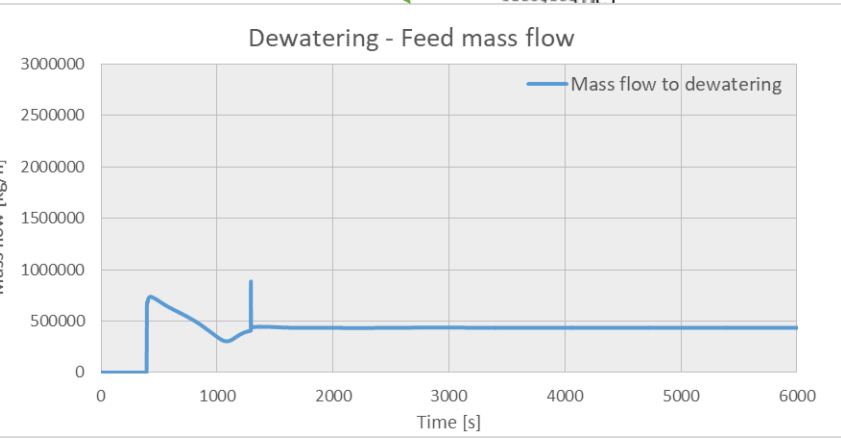
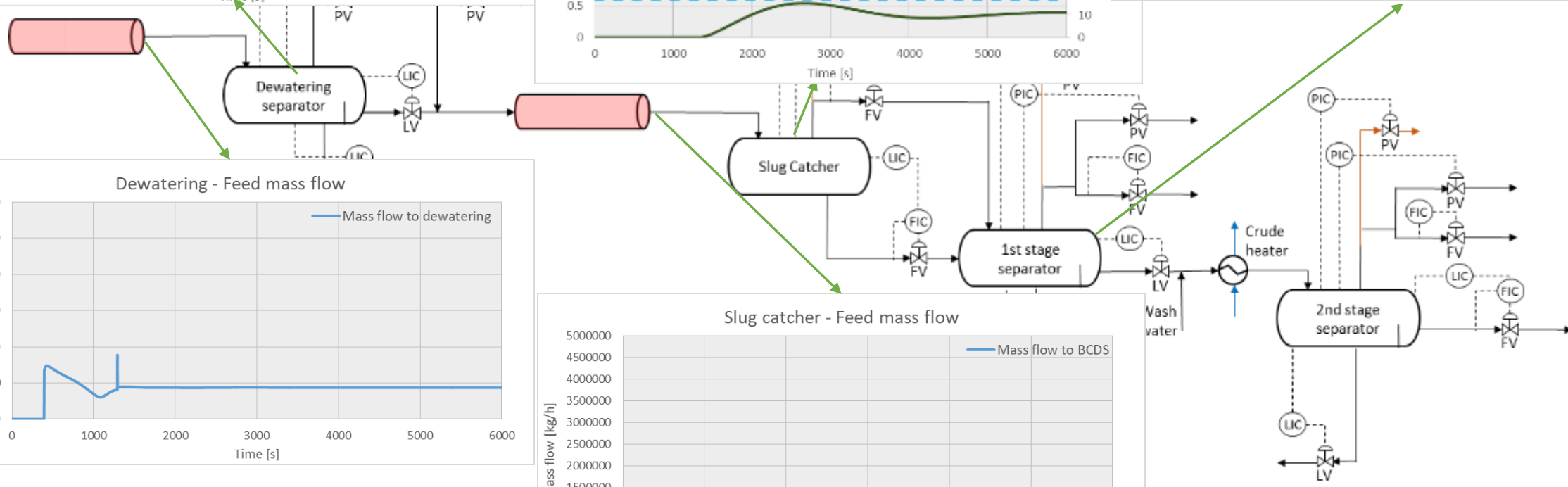
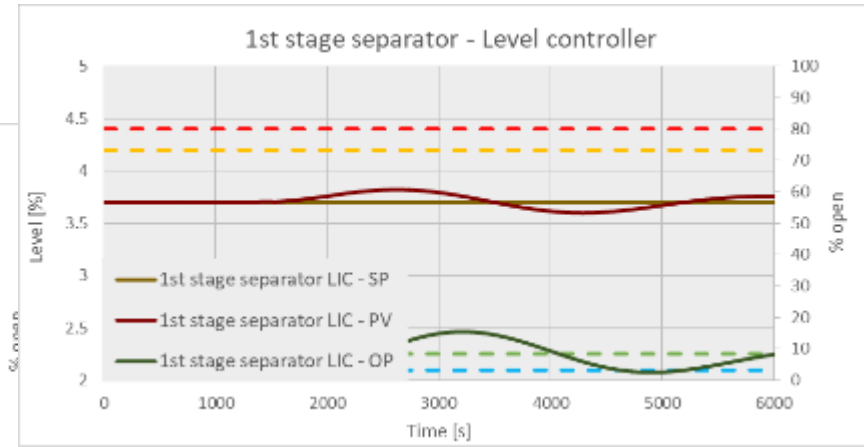
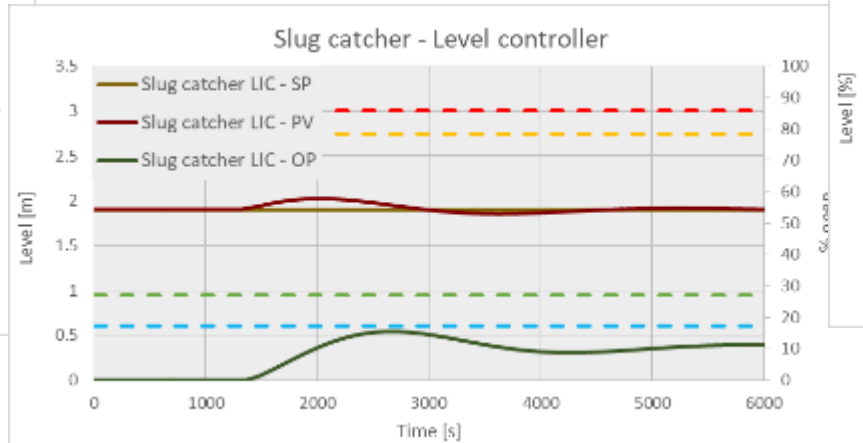
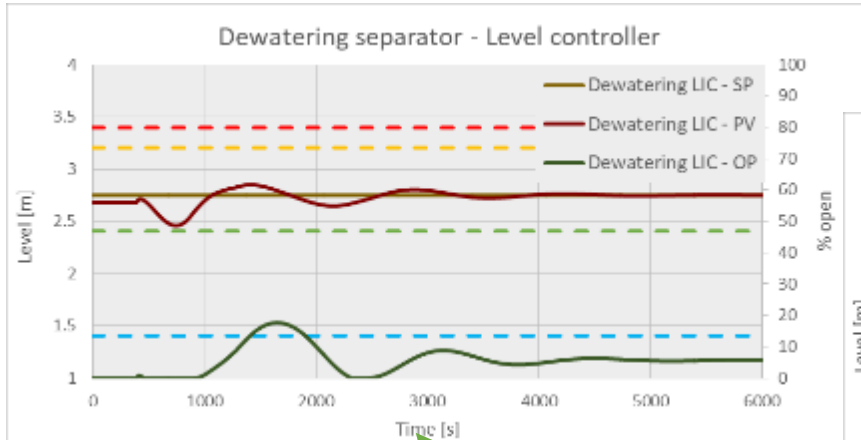
Stage Separators Initial Condition

- ✓ Isolation valves open
- ✓ Pressure controllers in auto
- ✓ Other Controllers in Manual

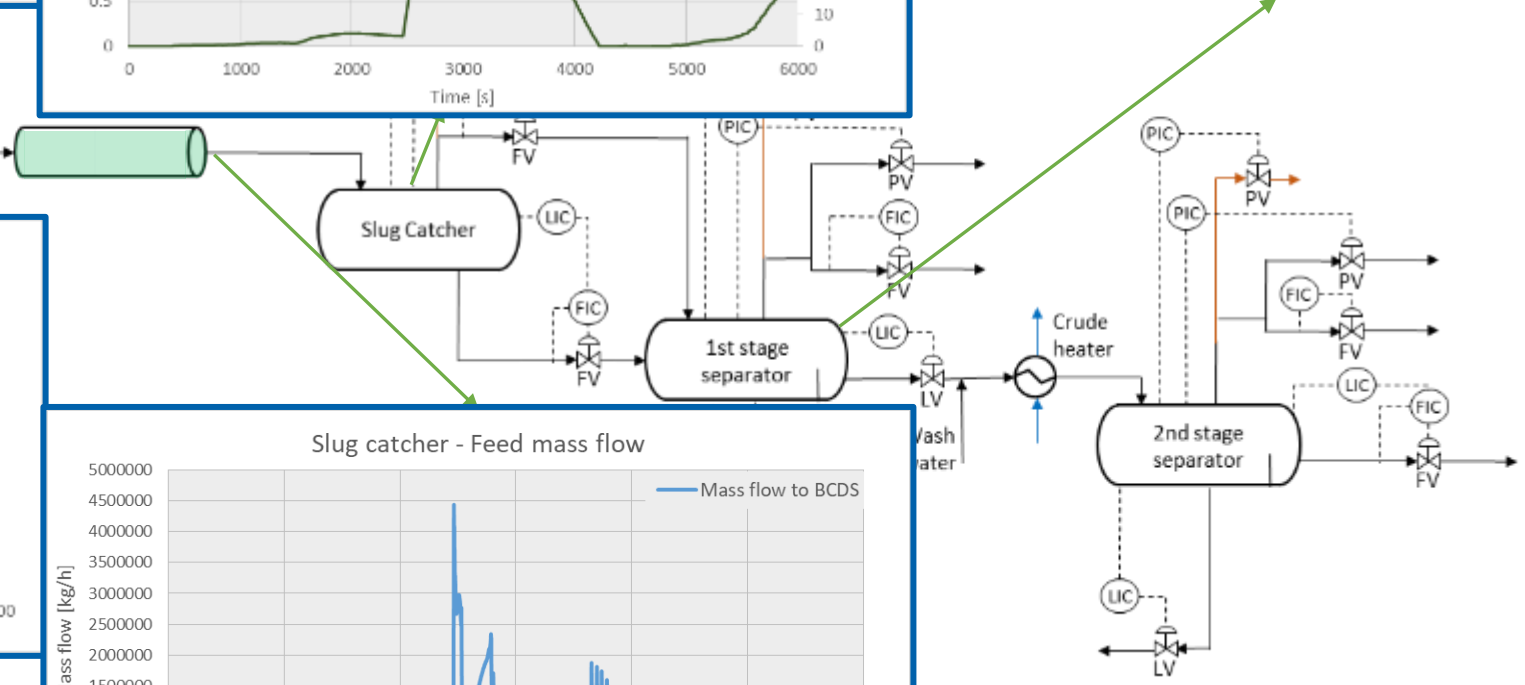
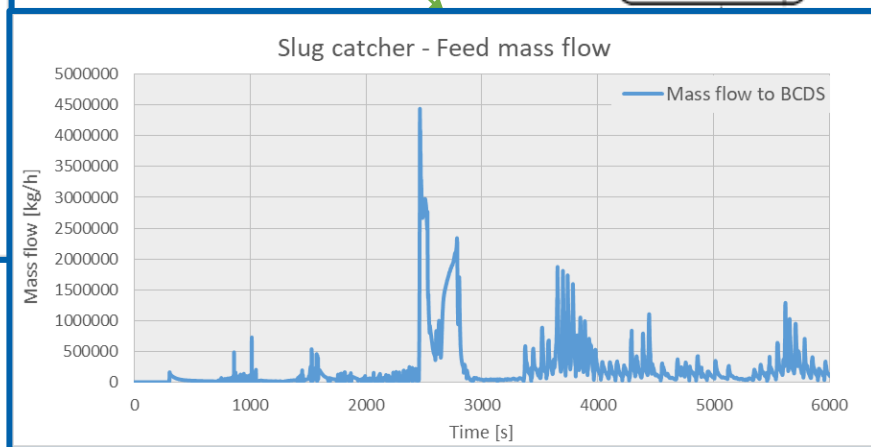
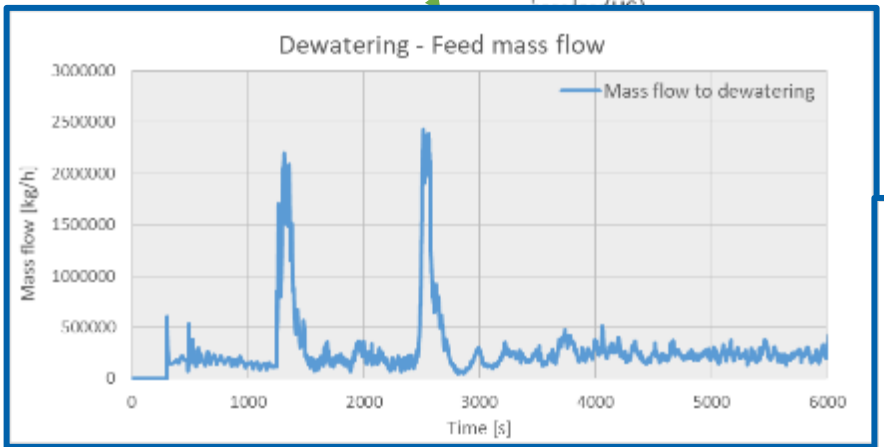
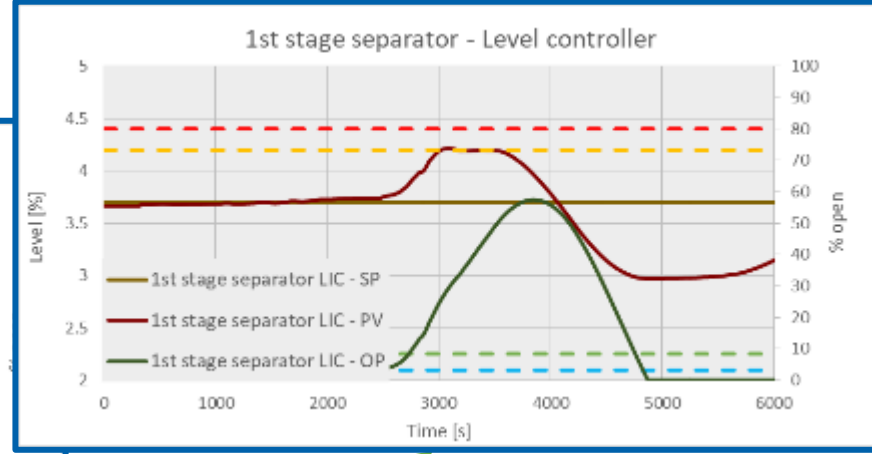
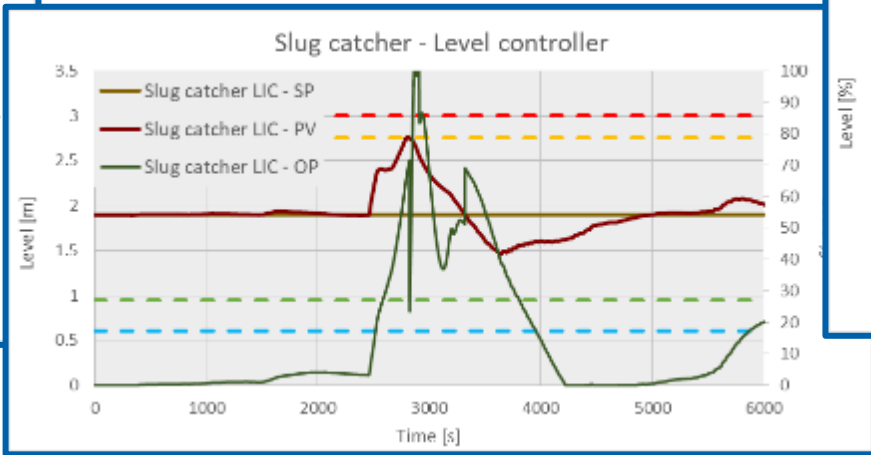
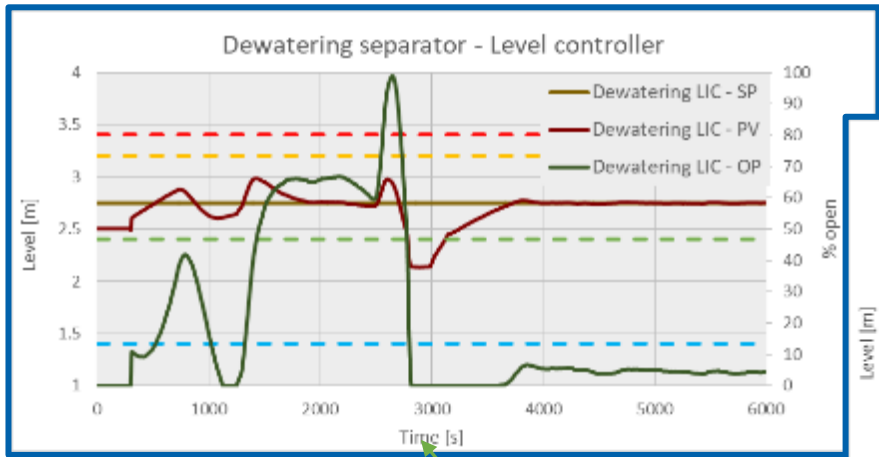
Procedure

1. Open inlet bypass valves
2. Open dewatering main isolation valve
3. Export oil from slug catcher
4. Export from 1st stage separator
5. Export from 2nd stage separator
6. Open full feed

*ESD- Emergency shut down



Start-up After ESD – Results (integrated models)



General conclusions

- Updated control set-up avoided trips in the facilities during start-up
- Dewatering section was enabled to start-up in automatic mode

Facilities - Flowline Model integration benefits for start-up

- Optimized start-up procedure reduces the start-up time by around 40% (for a typical black start-up)
 - A net saving of 4 days can be achieved for steady state operation
 - Considering around 100,000 bbl/day production / oil price of \$50/bbl, this results in savings of \$20MM
- A surge to liquid reaches the facilities
 - Stage separators surge of liquid is quite high.
 - Controllers had to be more aggressive than expected during startup modelling without integration. Slugging behavior at dewatering station is observed. It is shown that facilities are able to handle the fluctuations produced.

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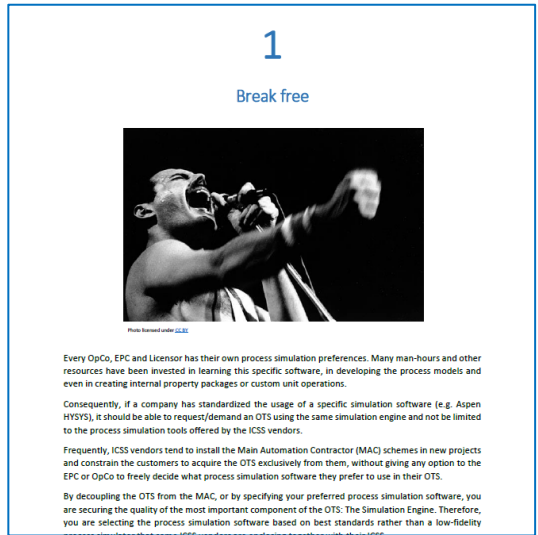
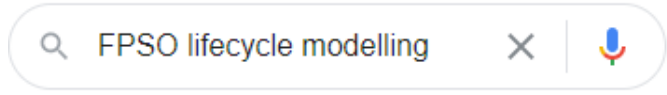
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World Oil article about applying Lifecycle modelling to Yinson JAK FPSO in Ghana



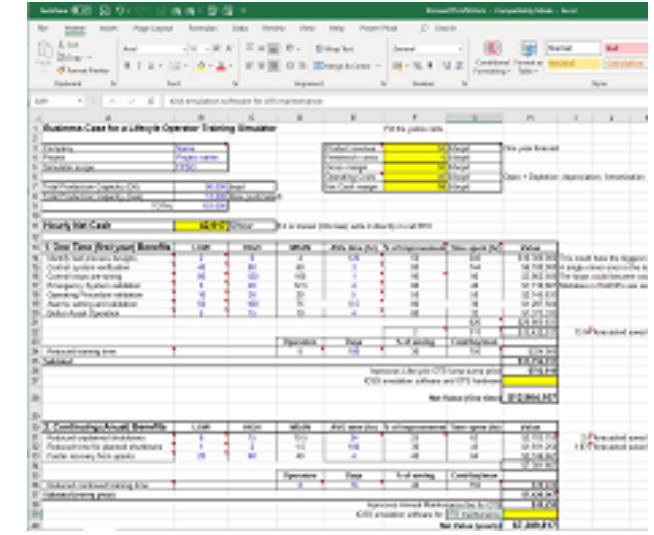
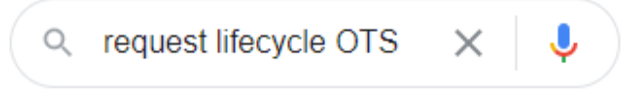
Visit our webpage, or



Easy to read Whitepaper about Best Practices to request and exploit Lifecycle OTSs / MPDS



Visit our webpage, or



Excel file with a configurable business case to justify a lifecycle Digital Twin investment



Send email to:
michael.brodkorb@inprocessgroup.com

Thank you!

Q&A



Oriol Millan



Michael Brodkorb

www.inprocessgroup.com

